

Temperature- and Salinity-Decoupled Overproduction of Hydroxyectoine by *Chromohalobacter salexigens*

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Hydroxyectoine overproduction by the natural producer *Chromohalobacter salexigens* is presented in this study. Genetically engineered strains were constructed that at low salinity coexpressed, in a vector derived from a native plasmid, the ectoine (*ectABC*) and hydroxyectoine (*ectD*) genes under the control of the *ectA* promoter, in a temperature-independent manner. Hydroxyectoine production was further improved by increasing the copies of *ectD* and using a *C. salexigens* genetic background unable to synthesize ectoines.

ctoine and hydroxyectoine (ectoines) are compatible solutes synthesized and accumulated by halophilic and halotolerant bacteria in response to osmotic and heat stress (1, 2). Ectoines have current applications as biostabilizers of proteins and nucleic acids, as well as a potential role as therapeutics for certain diseases (3, 4). This, together with the complexity of their chemical synthesis, has encouraged recent efforts to improve ectoine production from bacteria. Hydroxyectoine is especially interesting, as it seems to confer additional protections derived from its hydroxylated nature (3, 4). Ectoines are synthesized from aspartate semialdehyde. First, this metabolite is converted into diaminobutyric acid, which is acetylated to Ny-acetyldiaminobutyric acid and subsequently cycled to ectoine (5, 6). The main route of hydroxyectoine synthesis is via ectoine hydroxylation (2). The enzymes for ectoine synthesis are usually encoded in an ectABC-type gene cluster, which is usually well conserved among ectoine-producing microorganisms (7). There are exceptions, such as incomplete operons, gene clusters including the ask gene (for the aspartate kinase), gene clusters carrying ectABC-ectD-ask, and scattering of the genes within the chromosome, with duplications of ectC and ectD or even solitary ectC (5, 7, 8). Industrial production of hydroxyectoine uses Halomonas elongata ATCC 33173^T grown under high-salinity and high-temperature conditions, using the bacterial milking method (9), or a derivative of this technique (10), followed by separation and purification of ectoine and hydroxyectoine (9). This salt and temperature requirement for hydroxyectoine synthesis is a serious drawback of using natural producers, since fermentation under high temperature and salinity increases production costs and corrodes industrial reactors.

Chromohalobacter salexigens is a halophilic gammaproteobacterium which produces ectoine and hydroxyectoine in response to salt and heat stress, respectively (7). It is easy to grow and its genome sequence is available (http://genome.ornl.gov/microbial/csal/). It has been suggested as an alternative to H. elongata (11). In C. salexigens, the genes encoding ectoine synthesis lay within a 2.8-kb region encoding the diaminobutyric acid acetyltransferase (EctA), diaminobutyric acid transaminase (EctB), and ectoine synthase (EctC) (12). The microorganism has two paralogs of the enzyme ectoine hydroxylase, EctD and EctE, but EctD is the main responsible enzyme for hydroxyectoine production (2). In C. salexigens, the gene cluster ectABC and the genes ectD and ectE are at different loci within the chromosome.

Whereas accumulation of both solutes in C. salexigens is max-

imal during stationary phase, the accumulation of hydroxyectoine is upregulated by salinity and temperature, and the accumulation of ectoine is upregulated by salinity and downregulated by temperature. Thus, hydroxyectoine production and accumulation is maximum at 45°C and 14.5% NaCl, while ectoine accumulation reaches its maximum at 37°C and 17.4% NaCl (2). This regulation occurs, at least in part, at the transcriptional level. The ectoine synthesis genes ectABC can be expressed from two promoter regions, one located upstream of ectA and composed of four putative promoters (PectA1 to PectA4 [PectA1-4]) and a second internal promoter located upstream of ectB (PectB). In silico analysis of the -10 and -35 sequences of these regions showed that PectA1 and PectA2 may be dependent on the main vegetative factor σ^{70} (and therefore constitutively expressed), whereas PectA3 and PectB were similar to σ^{S} - and σ^{32} -dependent promoters, respectively. In agreement with these predictions, expression of a PectA1-4::lacZ fusion was osmoregulated and depended in part on the general stress factor σ^{S} , whereas PectB was induced by continuous growth at a high temperature (13). On the other hand, the promoter region of ectD is composed of two promoters (PectD1 and PectD2), and ectD expression is both osmo- and thermoregulated (M. Reina-Bueno, unpublished data).

In this work, we have metabolically engineered *C. salexigens* to overproduce hydroxyectoine at low salinity, in a temperature-independent manner. In order to maximize hydroxyectoine production and to minimize its temperature and salinity requirements, we designed transcriptional fusions between the ectoine synthesis genes *ectABC* and the main hydroxyectoine synthesis gene *ectD*, so that the second became transcriptionally controlled by the *ectABC* promoter region. To construct a functional *ectABCD* cassette, we first amplified by PCR a 3,384-bp sequence, including the promoter region upstream of *ectA*, the *ectABC* gene cluster, and the rho-independent terminator downstream of *ectC*,

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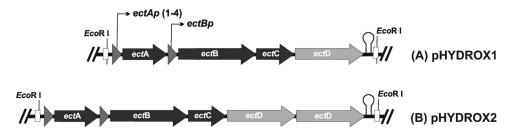


FIG 1 Genetic organization of constructed inserts, cloned in pHS15 to obtain pHYDROX1 (A) and pHYDROX2 (B).

and cloned it into pBluescript SK, resulting in pME2. Then, we inserted a BamHI restriction site between ectC and the rho-independent terminator by site-directed mutagenesis using the primer pair ectBam_fw and ectBam_rv (see Table S1 in the supplemental material for a list of primers used in this study). Subsequently, we eliminated the BamHI restriction site from the multicloning site of pBluescript SK using the primers QuitBam fw and QuitBam_rv, getting pME2.3. Next, we amplified a 1,200-bp sequence from the C. salexigens genome, including ectD, and inserted it into pBluescript SK, getting the plasmid pECTD. Then, we introduced a BclI restriction site downstream of *ectD* using the primers ectDBcl fw and ectDBcl rv, resulting in pECTD2. Subsequently, we excised promoterless ectD from pECTD2 by digesting it with BclI and inserted it in BamHIdigested pME2.3, yielding pECTABCD. Finally, the engineered ectABCD gene cluster was excised from pECTABCD by digestion with EcoRI and cloned into EcoRI-digested pHS15 (a cloning and expression vector based on a native plasmid from H. elongata harboring a streptomycin resistance gene [14]), obtaining pHYDROX1 (Fig. 1A). To increase the ectD gene dose, a second functional cassette, ectABCDD, was constructed. For this purpose, a second copy of ectD was cloned between ectD and the rho-independent terminator in the previous ect-ABCD-constructed gene cluster. First, we introduced a BamHI restriction site between ectD and the rho-independent terminator in pECTABCD, using the primers ABCDBam_fw and ABCDBam_rv, getting pME2.4. Then, an internal BamHI site of ectD was eliminated by introducing a silent mutation with the primers QuitBamD_fw and QuitBamD_rv, resulting in pME2.5. Next, ectD was excised from pECTD2 with BclI and cloned in BamHI-digested pME2.5, resulting in pECTABCDD. Subsequently, the ectABCDD synthetic gene cluster was excised by digestion with EcoRI from pECTABCDD and cloned in EcoRI-digested pHS15, resulting in pHYDROX2 (Fig. 1B). Both plasmids pHYDROX1 and pHYDROX2 were transformed into Escherichia coli DH5α cells, and the resulting strains were used as donors in a conjugation with C. salexigens wild type and mutant CHR137 ($\Delta ectABC::Tn1732$, $ectD::\Omega$; unable to synthesize ectoines) (2).

To evaluate hydroxyectoine production in both the natural producer *C. salexigens* and the heterologous host *E. coli* DH5α, we determined the ectoine content in all strains containing pHY-DROX1 and pHYDROX2. For this purpose, cells were grown at different temperatures (37°C for *E. coli* and 37, 40, and 45°C for *C. salexigens*) in shaking flasks with minimal medium M63 added with 20 mM glucose and different salinities (1%, 2%, or 3% NaCl for *E. coli* strains and 4.35%, 8.7%, or 14.5% NaCl for *C. salexigens* strains) until early stationary phase. Cellular extracts used for liq-

uid chromatography-mass spectrometry (LC-MS) and supernatants used for high-pressure liquid chromatography with UV detector (HPLC-UV) analysis of ectoine and hydroxyectoine were prepared by using a modified Bligh-Dyer technique described by Kraegeloh and Kunte (15). For cellular extracts, chromatographic separation and HPLC-electrospray ionization was performed as described by Argandoña et al. (16). For supernatants, samples were analyzed as described by García-Estepa et al. (2).

Hydroxyectoine levels observed in the heterologous recombinant strains E. coli DH5α/pHYDROX1 and E. coli DH5α/ pHYDROX2 grown at 1%, 2%, or 3% NaCl were very low, and only traces of ectoine were detected (data not shown). Table 1 summarizes growth rates and ectoine and hydroxyectoine production by the different *C. salexigens* wild-type and recombinant strains, as well as their specific production rates. As production of ectoines is directly related to the biomass produced at a certain salinity (11), the specific production rate (µmol/g bacterial dry matter [BDM] · h) is a simple function reflecting solute content and growth rate (17). As previously reported (2), ectoine accumulation by C. salexigens wild type was salinity dependent and, at a given salinity, inversely correlated to increasing temperature. Ectoine reached its maximal accumulation (725 µmol/g BDM) at 37°C with 14.5% of NaCl, with an ectoine/hydroxyectoine ratio of 2.24:1. On the other hand, hydroxyectoine accumulation by the wild type was salinity and temperature dependent, reaching its maximum at 45°C with 14.5% NaCl, with an ectoine/hydroxyectoine ratio of 0.45:1 and a yield of 942 µmol/g BDM.

All C. salexigens recombinant strains carrying plasmids pHYDROX1 or pHYDROX2, grown at 37°C or 40°C with 4.35% or 8.7% NaCl, showed much higher hydroxyectoine and much lower ectoine yields, respectively, than the wild-type strain carrying no plasmid under the same conditions. In all cases, the major product was hydroxyectoine, and the higher hydroxyectoine production was accompanied by a decrease of growth rates. This was correlated with the lower ectoine yields observed, confirming that ectoine is necessary for osmoprotection of C. salexigens. Otherwise, ectoine production by C. salexigens recombinant strains at 14.5% NaCl could not be measured, as they did not grow or showed only residual growth. For a given recombinant strain, growth at 40°C did not result in a significant increase of hydroxyectoine yield, if compared to the same strain grown at 37°C. This finding indicated that the higher hydroxyectoine synthesis in the engineered strains was mostly driven by the PectA promoter region and therefore decoupled from temperature control.

With the exception of cells grown at 40°C with 8.7% NaCl, in the wild-type background the presence of an extra copy of *ectD* (i.e., cells carrying pHYDROX2 versus cells carrying pHYDROX1 grown under the same conditions) did not improve hydroxyecto-

TABLE 1 Ectoine and hydroxyectoine yield and production rates of C. salexigens assayed strains^a

				Ectoine		Hydroxyectoine	
Strain	Temp (°C)	Salinity (%)	Growth rate (μh^{-1})	Yield (μmol/g BDM)	Specific production rate $(\mu \text{mol/g BDM} \cdot h)^b$	Yield (µmol/g BDM)	Specific production rate (µmol/g BDM · h)
C. salexigens DSM3043 wild type	37	4.35	0.24	393 ± 18.5	94.3	59 ± 2.9	14.1
	37	8.7	0.33	654 ± 27.6	215.8	202 ± 7.8	66.6
	37	14.5	0.21	725 ± 22.3	152.2	324 ± 11.3	68
	40	4.35	0.22	180 ± 8.5	39.6	23 ± 0.8	5.06
	40	8.7	0.30	449 ± 9.6	134.7	176 ± 7.8	52.8
	45	14.5	0.15	381 ± 12.2	57.21	942 ± 20	141
Wild type/pHYDROX1	37	4.35	0.14	220 ± 5.4	30.8	483 ± 9.9	67.62
	37	8.7	0.25	156 ± 3.1	39	424 ± 7.5	106
	40	4.35	0.12	48.5 ± 1.2	5.8	468 ± 8.2	56.16
	40	8.7	0.24	20.4 ± 0.4	4.9	255 ± 3.3	61.2
Wild type/pHYDROX2	37	4.35	0.18	68 ± 1.2	12.2	384 ± 6.8	69.12
,, ,	37	8.7	0.29	108 ± 2.4	31.3	361 ± 7.3	104.6
	40	4.35	0.17	48.85 ± 0.9	8.3	419 ± 9.3	71.23
	40	8.7	0.24	105 ± 3.4	25.2	354 ± 10.1	84.96
CHR137/pHYDROX1	37	4.35	0.14	81 ± 2.2	11.3	598 ± 12.8	83.72
•	37	8.7	0.1	170 ± 4.1	17	632 ± 14.5	63.2
	40	4.35	0.13	36.5 ± 1.4	4.7	478 ± 12.2	62.14
	40	8.7	0.1	90 ± 3.3	9	521 ± 16.4	52.1
CHR137/pHYDROX2	37	4.35	0.14	93 ± 2.9	13	883 ± 18.9	123.62
1	37	8.7	0.1	286 ± 5.8	28.6	967 ± 24.1	96.7
	40	4.35	0.12	67.5 ± 3.1	8.1	768 ± 31.2	92.1
	40	8.7	0.11	122.6 ± 4.5	13.48	805 ± 25.2	88.5

a Experiments were repeated twice with three independent measurements. The results are averages from the six measurements \pm standard deviations.

ine yield. In addition, an increase in salinity (i.e., the same recombinant strain grown at 8.7% versus 4.35% NaCl at a given temperature) did not improve hydroxyectoine production in the wildtype background. However, in the ectoine-deficient strain CHR137 (2), incrementing ectD dose or salinity did enhanced hydroxyectoine yields. These findings suggest that control mechanisms ruled by endogenous ectABC and/or ectD genes are somehow repressing hydroxyectoine synthesis in the wild-type background.

The best production results were achieved with strain CHR137 carrying pHYDROX2. This strain grown at 8.7% NaCl reached a hydroxyectoine yield of 967 µmol/g BDM (4.78-fold higher than that achieved by the wild-type strain at this salinity), with a total ectoine yield of 1,253 µmol/g BDM (ectoine/hydroxyectoine ratio of 0.29:1) and a significant decrease of the growth rate (0.1 h⁻¹) that reduced the specific production rate to 96.7 μ mol/g BDM · h. However, the same strain grown at 4.35% NaCl showed a hydroxyectoine yield of 883 µmol/g BDM (14.96-fold higher than that observed in the wild-type strain at the same salinity), maintaining a reasonable growth rate (0.14 h⁻¹, with a specific production rate of 123.6 µmol/g BDM · h) and reaching an ectoine/ hydroxyectoine ratio of 0.1:1. These production data at low salinity and optimal temperature are very similar to those shown by the wild type grown at high salinity and high temperature (14.5% NaCl and 45°C).

In most bacteria, the responses to osmotic and/or heat stress involve the synthesis of a cocktail of compatible solutes (7). Thus, the presence of by-products other than ectoine was investigated in

the most promising strain, CHR137/pHYDROX2, grown at 37°C with low salinity and compared to the cytoplasmic solute pool synthesized by the wild type carrying either pHYDROX2 or no plasmid. As shown in Fig. S1 in the supplemental material, the major compatible solute in C. salexigens wild-type cells grown at 37°C with 4.35% NaCl was ectoine, followed by glutamate and minor amounts of glucosylglycerol and hydroxyectoine. Introduction of pHYDROX2 in wild-type cells switched the synthesis to hydroxyectoine, which became the major compatible solute, followed by glutamate, trehalose, and minor amounts of glucosylglycerol and ectoine. The presence of trehalose in the wild type overexpressing hydroxyectoine at 37°C was unexpected, as this sugar is synthesized by C. salexigens in response to heat stress or when ectoine is absent (18). This apparent induction of trehalose synthesis by hydroxyectoine will be investigated in a further work. Finally, transfer of pHY-DROX2 to the ectoine-deficient strain CHR137 led to a much cleaner compatible solute profile, consisting of mainly hydroxyectoine and reduced amounts of glutamate and trehalose. Ectoine was not detected, although it should be present in minor amounts, as judged by our previous estimations (Table 1).

In general, two alternative biological systems would be suitable to approach hydroxyectoine production: nonhalophilic microorganisms bearing hydroxyectoine synthesis genes and natural (halophilic) producers, either cultured in optimized conditions for solute production or metabolically engineered for hydroxyectoine overproduction (4). Table 2 summarizes most of the so-farreported hydroxyectoine production systems, including relevant

^b BDM, bacterial dry matter.

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TABLE 2 Comparison of hydroxyectoine production systems

jundiciproducers jundic	Strain	Temp (°C)	Salinity (%)	Growth phase	Growth rate (μh^{-1})	OH-ectoine yield (µmol/g BDM)	Specific OH-ectoine production rate (µmol/gBDM·h) ^a	Byproduct(s)	Reactor system	Product extraction	Reference
37 1.74 After 16 hof NR 29.95 NR Ectoine (107 μnnol/g BDM), other Barch Methanol-chloroform extraction solutes not tested solutes not tested solutes not extend solutes and tested solutes not extend solutes and tested solutes not extend solutes and tested solutes not extend solutes not extend solutes and tested solutes not extend solu	Nonhalophilic producers E. coli DH5α/pSB01 ^b	37	2.0	Late stationary	0.35	500	175	Trehalose ectoine (<5%)	Batch	Methanol-chloroform extraction	17
37 1.74 After 16 h of incabation NR 91 NR Ectoine (107 μπολής BDM), other Batch incabation with incabation NR 91 NR Ectoine (107 μπολής BDM), other Batch Methanol-chloroform extraction solutes not texted in the proposed of the proposed o	E. coli FF4169/pNST5 ^c	37	1.74	After 16 h of incubation	NR^k	29.95	NR	Ectoine (10.32 μmol/g BDM), other solutes not tested	Batch		19
2 35 10.0 Stationary 0.25 860 215 Glutamate 2 37 10.0 Stationary 0.20 670 134 2 37 10.0 Stationary 0.03 603 18 2 37 10.0 Stationary 0.03 603 18 2 37 10.0 Stationary 0.03 603 18 3173 ^T 25 18.5 Stationary 0.04 28 NR Ectoine, PHB Two-left-batch' Thermal permeabilization 3173 ^T 25 15 Exponential 0.04 28 NR Ectoine, PHB Two-left-batch Thermal permeabilization 3173 ^T 25 15 Exponential NR 290 NR Ectoine (762 μmol/g BDM), Nγ- glutamate, alamine, other amino acids 3173 ^T 40 15 Late exponential NR 290 NR Ectoine (762 μmol/g BDM), Batch Methanol-chloroform extraction 3173 ^T 40 20 Late exponential NR 290 NR Ectoine (762 μmol/g BDM), SDSM 37 14.5 Early stationary 0.15 942 141 Ectoine (273 μmol/g BDM), SDSM 37 10.5 Exponential 0.3 2.528 76 Ectoine (372 μmol/g BDM), SDSM 37 10.6 Exponential NR 367 NR Ectoine (372 μmol/g BDM), other cell receitors SDSM 37 10.0 Exponential NR 364 69.12 Ectoine, other solutes not determined SDSM 37 10.0 Exponential NR 364 69.12 Glutamate, rehalose, NAGGN Batch Methanol-chloroform extraction Methanol-chloroform extraction Methanol-chloroform extraction SDSM 37 10.0 Exponential NR 364 69.12 Glutamate, irrehalose, NAGGN Batch Methanol-chloroform extraction SDSM 37 10.0 Exponential NR 364 69.12 Glutamate, irrehalose, extoine, Batch Methanol-chloroform extraction Mid-exponential NR 364 69.12 Glutamate, irrehalose, extoine, Batch Methanol-chloroform extraction Methanol-chloroform extract	E. coli FF4169/pNST6 ^d	37	1.74	After 16 h of incubation	NR	91	NR	Ectoine (107 μ mol/g BDM), other solutes not tested	Batch		19
2 35 10.0 Stationary 0.25 86.0 215 Glutamate Fed-batch' Methanol-chboroform extraction Batch-fed-batch' Thermal permeabilization Batch Gel-batch Downshods accept diaminate plutose glutamate, alanine, other amino activate plutose glutamate, glutose subtamate, glutose glutamate, glutose subtamate, glutose glutamate, glutose glutamate, glutose glutamate, glutose glutamate, glutose glutamate, glutose glutamate, glutose subtamate, glutose glutamate, glutose glutamate, glutose subtamate, glutose glutamate, glutose glutamate, glutose subtamate, glutose subtamate, glutose subtamate, glutose glutamate, glutose subtamate, glutose subta	Natural producers										
2 37 10.0 Stationary 0.20 670 134 2 37 10.0 Stationary 0.03 603 18 3 10.0 Stationary 0.04 28 NR Ectoine (1.462 μmol/g BDM), Nγ- Barch-fed-batch Downshods acetyldiamino-butyric acid, glutamate, alanine other amino acids planally glutamate, glucose 10 planally glutamate, glutamate, glucose 10 planally glutamate, glut	Marinococcus sp. strain M52	35	10.0	Stationary	0.25	860	215	Glutamate	Fed-batch-batche		20
2 37 10.0 Stationary 0.03 603 18 35 18.5′ Stationary Multistep 950 169 Ectoine, PHB Two-step 10-ownshocks 128 Stationary 129 169 Ectoine (1,462 μπου/g BDM), Nγ- Each-fed-batch Downshocks 28 Recoine (1,462 μπου/g BDM), Nγ- Each-fed-batch Downshocks 28 Ectoine (1,462 μπου/g BDM), Nγ- Each-fed-batch Downshocks 28 Ectoine (762 μπου/g BDM), Spring 129 129 129 129 129 129 129 129 129 129	Marinococcus sp. strain M52	37	10.0	Stationary	0.20	670	134		Batch-fed-batch ^e		21
35 18.5′ Stationary Multistep 950 169 Ectoine, PHB Two-step led-batch process (Fed-batch process) and process (Fed-batch process (Fe	Marinococcus sp. strain M52	37	10.0	Stationary	0.03	603	18		Batch-fed-batch ^e		21
33173 ^T 25 15 Exponential 0.04 28 NR Ectoine (1.46; μmol/g BDM), Nγ- acicly glutamate, glamine, other amino 33173 ^T 30 10.0 Late exponential NR 290 NR Ectoine (762; μmol/g BDM), 33173 ^T 40 15 Late exponential NR 290 NR Ectoine (764) μmol/g BDM), 33173 ^T 40 20 Late exponential NR 290 NR Ectoine (784 μmol/g BDM), 33173 ^T 40 20 Late exponential NR 290 NR Ectoine (786 μmol/g BDM), 33173 ^T 40 15 Early stationary 0.21 324 68 Ectoine (786 μmol/g BDM), 33183 14.5 Early stationary 0.15 942 141 Ectoine (781 μmol/g BDM), 345 Late exponential NR 367 NR Ectoine (781 μmol/g BDM), 350 Exponential NR 367 NR Ectoine (781 μmol/g BDM), 367 NR Ectoine (781 μmol/g BDM), 370 Late exponential NR 367 NR Ectoine (781 μmol/g BDM), 388 Solute mate, plucose 3918 20 Late exponential NR 367 NR Ectoine (781 μmol/g BDM), 389 Exponential NR 367 NR Ectoine (781 μmol/g BDM), 390 Exponential NR 367 NR Ectoine, trehalose, NAGGN Batch Methanol-chloroform extraction 39190 ^T 37 4.0 Mid-exponential NR 367 NR Ectoine, other solutes not determined 39190 NR 2010 Early stationary NR 100′ NR 0% ectoine, trehalose, NAGGN Batch Methanol-chloroform extraction 39180 NR 2010 Early stationary NR 100′ NR 0% ectoine, other solutes not extraction Methanol-chloroform extraction 39180 NR 2010 Early stationary NR 100′ NR 0% ectoine, other solutes not extraction Methanol-chloroform extraction 39180 NR 0% ectoine, other solutes not extraction Methanol-chloroform extraction 39180 NR 0% ectoine, other solutes not extraction Methanol-chloroform extraction 39180 NR 0% ectoine, other solutes not extraction Methanol-chloroform extraction 39180 NR 0% ectoine, other solutes not extraction Methanol-chloroform extraction 39180 NR 0% ectoine, other solutes not extraction Methanol-chloroform extraction 39180 NR 0% ectoine, other solutes not extraction Methanol-chloroform extraction 39180 NR 0% ectoine, other solutes not extraction Methanol-chloroform extraction 39180 NR 0% ectoine, other solutes not extraction Methanol-chloroform extraction 39180 NR 0% ectoine, other solute	Halomonas boliviensis	35	18.5 ^f	Stationary	Multistep process	950	169	Ectoine, PHB	Two-step fed-batch		22
33173 ^T 30 10.0 Late exponential 0.242 36 8.71 Ectoine (762 μmol/g BDM), Batch Chloroform extraction glutamate, glucose s DSM 35173 ^T 40 20 Late exponential NR 299 NR Ectoine (764 μmol/g BDM), Batch Methanol-chloroform extraction glutamate, glucose s DSM 37 14.5 Early stationary 0.21 324 68 Ectoine (725 μmol/g BDM), glutamate glucose s DSM 45 14.5 Early stationary 0.21 324 68 Ectoine (725 μmol/g BDM), glutamate batch Methanol-chloroform extraction glutamate, glucose Ectoine (725 μmol/g BDM), glutamate batch Methanol-chloroform extraction glutamate, glucose Ectoine (725 μmol/g BDM), glutamate batch Methanol-chloroform extraction glutamate, glucose and glutamate, glucose solution (725 μmol/g BDM), glutamate batch Methanol-chloroform extraction glutamate, glucose and glutamate, glucose solution (725 μmol/g BDM), glutamate batch Methanol-chloroform extraction glutamate, glucose and glutamate, glucose solution (725 μmol/g BDM), glutamate batch Methanol-chloroform extraction glutamate, glucose solution (725 μmol/g BDM), glutamate batch Methanol-chloroform extraction glutamate, glucose solution (725 μmol/g BDM), glutamate batch Methanol-chloroform extraction glutamate, glucose solution (725 μmol/g BDM), glutamate batch Methanol-chloroform extraction glutamate, glucose colline, glutamate, glucose solution solution solution solution glutamate, glucose solution (725 μmol/g BDM), glutamate batch Methanol-chloroform extraction glutamate, glucose colline, glutamate, glucose solution	Halomonas elongata ATCC 33173 ^T	25	15	Exponential	0.04	28	NR	Ectoine (1,462 µmol/g BDM), Ny- acetyldiamino-butyric acid, glutamate, alanine, other amino acids	Batch-fed-batch		9
33173 ^T 40 15 Late exponential NR 290 NR Ecroine (740 μπου/g BDM), Batch Methanol-chloroform extraction glutamate, glucose 33173 ^T 40 20 Late exponential NR 440 NR Ectoine (860 μπου/g BDM), Batch Methanol-chloroform extraction glutamate, glucose s DSM 37 14.5 Early stationary 0.21 324 68 Ectoine (725 μπου/g BDM), glutamate Batch Methanol-chloroform extraction glutamate, rehalose, Nγ- accept/diamino-butyric acid s DSM 37 10.75 Exponential 0.3 2.528 76 Ectoine, trehalose, NAGGN Batch Downshocks solutes not determined elementions s DSM 37 10 Early stationary NR 367 NR Ectoine, trehalose, NAGGN Batch Methanol-chloroform extraction s DSM 37 10 Early stationary NR 100 NR DSM, ectoine, trehalose, NAGGN Batch Methanol-chloroform extraction s DSM 37 4.35 Early stationary 0.18 384 69.12 Glutamate, trehalose, glycolsyiglycerol, Batch Methanol-chloroform extraction pμπου/g BDM), blutamate Batch Methanol-chloroform extraction s DSM 37 10 Early stationary NR 100 NR OS ectoine, trehalose, NAGGN Batch Methanol-chloroform extraction s DSM 37 4.35 Early stationary 0.18 883 123.62 Glutamate, trehalose, glycolsyiglycerol, Batch Methanol-chloroform extraction pμπου/g BDM) Batch Methanol-chloroform extraction s DSM 37 4.35 Early stationary 0.14 883 123.62 Glutamate, trehalose, ectoine (93 Batch Methanol-chloroform extraction pumo/g BDM)	Halomonas elongata ATCC 33173 ^T	30	10.0	Late exponential	0.242	36	8.71	Ectoine (762 μmol/g BDM), glutamate, glucose	Batch		23
33173 ^T 40 20 Late exponential NR 440 NR Ectoine (860 molig BDM), Batch Methanol-chloroform extraction glutamate, glucose s DSM 37 14.5 Early stationary 0.21 324 68 Ectoine (725 μmol/g BDM), glutamate Batch Methanol-chloroform extraction s DSM 45 14.5 Early stationary 0.15 942 141 Ectoine (381 μmol/g BDM), glutamate Batch Methanol-chloroform extraction glutamate, trehalose, Nγ- accept/diamino-butyric acid solutes not determined solutes not determined Methanol-chloroform extraction p-2R ^h 37 10 Early stationary NR 100 ⁱ NR Ectoine, trehalose, NAGGN Batch Methanol-chloroform extraction p-2R ^h 37 10 Early stationary NR 100 ⁱ NR 0% ectoine, other solutes not determined ectoine ectoine ectoine glutamate, trehalose, glycolsy/glycerol, Batch Methanol-chloroform extraction p-2R ^h 37 4.35 Early stationary 0.18 883 123.62 Glutamate, trehalose, ectoine (93 Batch Methanol-chloroform extraction p-2R ^h 37 4.35 Early stationary 0.14 883 123.62 Glutamate, trehalose, ectoine (93 Batch Methanol-chloroform extraction p-2R ^h Me	$\it Halomonas elongata ATCC 33173^{ m T}$	40	15	Late exponential	NR	290	NR	Ectoine (740 µmol/g BDM), glutamate, glucose	Batch		24
sDSM 45 14.5 Early stationary 0.21 324 68 Ectoine (725 μmol/g BDM), glutamate Batch Methanol-chloroform extraction s DSM 45 14.5 Early stationary 0.15 942 141 Ectoine (381 μmol/g BDM), Batch Methanol-chloroform extraction glutamate, trehalose, Nγ-acetyldamino-butyric acid Ectoine (3.797 μmol/g BDM), other Continuous with Downshocks solutes not determined solutes not determined Ectoine, trehalose, NAGGN Batch Methanol-chloroform extraction Methanol-chloroform extraction Methanol-chloroform extraction Methanol-chloroform extraction Methanol-chloroform extraction determined STYDROX2 ^j 37 4.35 Early stationary 0.18 384 69.12 Glutamate, trehalose, glycolsylglycerol, Batch Methanol-chloroform extraction μmol/g BDM) Batch Methanol-chloroform extraction Methanol-chloroform extraction Methanol-chloroform extraction determined SIGNAC SIGN	Halomonas elongata ATCC 33173 ^T	40	20	Late exponential	NR	440	NR	Ectoine (860 µmol/g BDM), glutamate, glucose	Batch		24
s DSM 45 14.5 Early stationary 0.15 942 141 Ectoine (381 μmol/g BDM), glutamate, trehalose, Nγ- s cylidiamino-butyric acid s DSM 37 10.75 Exponential 0.3 2,528 76 Ectoine (3,797 μmol/g BDM), other cell retention* s DSM 37 10.75 Exponential 0.16 480 76.8 Ectoine, trehalose, NAGGN BBDM), other cell retention* s DSM 37 4.0 Mid-exponential NR 367 NR Ectoine, trehalose, NAGGN Batch Methanol-chloroform extraction p-2R ^h 37 10 Early stationary NR 100' NR O% ectoine, other solutes not determined determined AYDROX2' 37 4.35 Early stationary 0.18 384 69.12 Glutamate, trehalose, glycolsylglycerol, Batch Methanol-chloroform extraction p-2R ^h 38 Early stationary 0.14 883 123.62 Glutamate, trehalose, ectoine (93 Batch Methanol-chloroform extraction μmol/g BDM) Methanol-chloroform extraction μmol/g BDM) Methanol-chloroform extraction μmol/g BDM)	Chromohalobacter salexigens DSM 3043 ^T	37	14.5	Early stationary	0.21	324	68	Ectoine (725 µmol/g BDM), glutamate	Batch		13; this study
s DSM 37 10.75 Exponential 0.3 2,528 76 Ectoine (3,797 μmol/g BDM), other continuous with pownshocks solutes not determined cell retentions determined cell retentions determined solutes not determined patch determined solutes not determined batch determined solutes not determined patch determined patch determined solutes not determined patch determined solutes not solutes not patch determined determined solutes not determined solutes not determined determined solutes not determined solution ectoine solutes not determined solutions (3,797 μmol/g BDM), other Continuous with Downshocks solutions (43,797 μmol/g BDM), other Continuous with Downshocks solutions solutions solutions solutions solutions solutions solutions (43,797 μmol/g BDM), other Continuous with Downshocks solutions (43,797 μmol/g BDM), other Continuous with Downshocks solutions (44,800 μmol/chloroform extraction μmol/g BDM).	Chromohalobacter salexigens DSM 3043 ^T	45	14.5	Early stationary	0.15	942	141	Ectoine (381 µmol/g BDM), glutamate, trehalose, N⁄y-acetyldiamino-butyric acid	Batch		2; this study
190 ^T 37 5.0 Exponential 0.16 480 76.8 Ectoine, trehalose, NAGGN Batch Methanol-chloroform extraction 190 ^T 37 4.0 Mid-exponential NR 367 NR Ectoine, trehalose, NAGGN Batch Methanol-chloroform extraction 192R ^h 37 10 Early stationary NR 100 ⁱ NR 0% ectoine, other solutes not determined 192ROX2 ⁱ 37 4.35 Early stationary 0.18 384 69.12 Glutamate, trehalose, glycolsylglycerol, Batch Methanol-chloroform extraction 193ROX2 ⁱ 37 4.35 Early stationary 0.14 883 123.62 Glutamate, trehalose, ectoine (93 Batch Methanol-chloroform extraction μποl/g BDM)	Chromohalobacter salexigens DSM 3043^{T}	37	10.75	Exponential	0.3	2,528	76	Ectoine (3,797 μmol/g BDM), other solutes not determined	Continuous with cell retention ^g	Downshocks	11
P-2R ^h 37 10 Early stationary NR 100 ⁱ NR 69.12 Glutamate, trehalose, ectoine (93 Batch Drome extraction Batch Drome extraction Batch Drome extraction Batch Drome extraction p-00.22 ⁱ 37 4.35 Early stationary 0.14 883 123.62 Glutamate, trehalose, ectoine (93 Batch Methanol-chloroform extraction p-mol/g BDM)	P seudomonas stutzeri DSM 5190^{T}	37	5.0	Exponential	0.16	480	76.8	Ectoine, trehalose, NAGGN	Batch		17
P-2R ^h 37 10 Early stationary NR 100 ⁱ NR 0% ectoine, other solutes not Batch Downshocks determined 4YDROX2 ⁱ 37 4.35 Early stationary 0.18 384 69.12 Glutamate, trehalose, glycolsylglycerol, Batch Methanol-chloroform extraction proximate p	Pseudomonas stutzeri A1501	37	4.0	Mid-exponential	NR	367	NR	Ectoine, trehalose, NAGGN	Batch		19
 X2' 37 4.35 Early stationary 0.18 384 69.12 Glutamate, trehalose, glycolsy/glycerol, Batch Methanol-chloroform extraction ectoine 37 4.35 Early stationary 0.14 883 123.62 Glutamate, trehalose, ectoine (93 Batch Methanol-chloroform extraction μποι/g BDM) 	Engineered natural producers <i>C. salexigens</i> DSM 3043 ^T /pJP-2R ^h	37	10	Early stationary	NR	100 ⁱ	NR	0% ectoine, other solutes not determined	Batch		25
37 4.35 Early stationary 0.14 883 123.62 Glutamate, trehalose, ectoine (93 Batch Methanol-chloroform extraction μ.mol/g BDM)	C. salexigens DSM 3043 ^T /pHYDROX2		4.35	Early stationary	0.18	384	69.12		Batch		This study
	C. salexigens CHR137/pHYDROX2	37	4.35	Early stationary	0.14	883	123.62	Glutamate, trehalose, ectoine (93 µmol/g BDM)	Batch		This study

[&]quot;Maximum specific hydroxyectoine production rates were calculated on the basis of growth rates and biomass content.

^d Trehalose-deficient E. coli carrying the ectABCDasK genes from P. stutzeri A1501. ^c Trehalose-deficient E. coli carrying the ectABCD genes from P. stutzeri A1501.

f Cells were first grown during 24 h at optimal salinity for biomass production (4.5% NaCl) and then transferred to a high-salinity medium (with 18.5% NaCl) for ectoines production.

h Carrying the thpD (ectD) gene, encoding the ectoine hydroxylase from Streptomyces crysomallus g Calculations for a maximum biomass of 61 g/liter. Fermentation was optimized for a simultaneous production of ectoine and hydroxyectoine.

¹ Carrying the ectABCDD cassette from C. salexigens DSM 3043 Percentage of ectoine conversion to hydroxyectoine; absolute yield not reported.

^k NR, not reported.

parameters such as growth conditions, hydroxyectoine yield and production rate, by-products, reactor systems, and product extraction procedures used. In this work, attempts to overproduce the C. salexigens ectABCD hydroxyectoine synthesis genes in E. coli DH5α were unsuccessful. It is possible that, as observed by Bestvater et al. (26) for the heterologous production of the Marinococcus halophilus ectoine synthesis genes, our heterologous production system might be improved by coexpressing a feedbackinsensitive aspartate kinase. This metabolic bottleneck was not found in the two reports so far describing successful hydroxyectoine production by E. coli carrying the hydroxyectoine synthesis genes from Pseudomonas stutzeri. However, differences in the osmotolerance conferred to the host strain, hydroxyectoine yield, presence of by-products, and the dependence of coexpresion of the ask gene for enhanced ectoine/hydroxyectoine production were found (17, 19) (Table 2), Thus, the trehalose-deficient E. coli strain FF4169 bearing the P. stutzeri A1501 ectABCD genes accumulated moderate levels of ectoine and hydroxyectoine, and the introduction of the ask gene (encoding an aspartate kinase specialized for ectoine/hydroxyectoine synthesis) led to a very strong increase in the contents of both solutes (Table 2). In both cases, host cells were osmoprotected (19). In contrast, E. coli DH5 α carrying the ectABCDask gene cluster from P. stutzeri DSM 5190^T synthesized almost exclusively hydroxyectoine as compatible solute (with about 5% of ectoine and trehalose), although conversion of ectoine into hydroxyectoine was delayed until late stationary phase. Surprisingly, this strain was not osmotolerant, and enhanced hydroxyectoine production was not dependent on coexpression of the aspartate kinase (17). Despite all this, hydroxyectoine content was much higher than that observed in the natural producer, with a yield of 500 µmol/g BDM (at stationary phase) and a specific production rate of 175 μmol/g BDM · h at 37°C and 2% NaCl. Compared to this strain, the specific hydroxyectoine production rate of C. salexigens CHR137/pHYDROX2 grown at the same temperature with 4.35% NaCl was slightly lower [123.6 μ mol/g BDM · h], but the hydroxyectoine yield was much higher (883 μmol/g BDM) (Table 2).

For the industrial production of hydroxyectoine, robust microorganisms with a broad salt tolerance are favored to perform the bacterial milking process (3, 4). Methods based on the Grampositive Marinococcus sp. strain M52 (20, 21) yielded considerable hydroxyectoine amounts at 37°C (Table 2) but had two disadvantages: (i) they cannot be milked by simple dilution of the medium, and (ii) they produce growth-inhibiting components such as acetate, which impede their use in batch and batch fermentation processes, unless complex techniques are utilized. Among Gramnegative bacteria of the *Halomonadaceae* family, *C. salexigens* (2), *H. boliviensis* (22), and *H. elongata* (9, 24) naturally produce more ectoine than hydroxyectoine, and increasing the hydroxyectoine content implies high-temperature and -salinity growth conditions (Table 2), with the disadvantages that these extreme conditions have for any industrial production system. In contrast, in P. stutzeri, hydroxyectoine is the predominant compatible solute at normal temperature (Table 2), and this microorganism has been suggested as an interesting candidate for the biotechnological production of hydroxyectoine (19).

At present, hydroxyectoine is produced on an industrial scale with *H. elongata* ATCC 33173^T (same as *H. elongata* DSM 2581^T). Both *C. salexigens* DSM 3043^T (strain 1H11; formerly named *H. elongata* DSM 3043) and *H. elongata* ATCC 33173^T (strain1H9)

were isolated by Vreeland et al. from a solar salt facility at Bonaire Island and initially assigned to H. elongata (27). On the basis of their phenotypic differences and their phylogenetic distance, strain H. elongata DSM 3043 was proposed as a new species of the genus Chromohalobacter and designated C. salexigens (7). Although both species show a similar temperature range (from 15 to 45°C, with optimum at 37°C) and optimal salinity (8.7 to 11.6% NaCl) for growth (28, 29), C. salexigens DSM 3043 seems to have more stringent requirements for salt. Thus, while the *H. elongata* type strain grew well with 0.3% NaCl in a minimal medium which is similar to M63 (29), C. salexigens could not grow at all in M63 unless it contained 2.9% NaCl (28). There are few reports describing hydroxyectoine production by H. elongata. Early studies by Wohlfarth et al. (24) and Severin et al. (23) showed increasing hydroxyectoine content in *H. elongata* in response to salinity and temperature, with 290 µmol/g BDM of hydroxyectoine (and 740 µmol/g BDM of ectoine) in cells grown in glucose mineral medium at 40°C with 15% NaCl (Table 2). This yield is lower than the hydroxyectoine accumulated by the *C. salexigens* wild-type strain at 37 or 45°C with a similar salinity (Table 2). Unfortunately, hydroxyectoine production by H. elongata at temperatures higher than 40°C or specific hydroxyectoine production rates at 40°C or higher were not reported, making it difficult to compare production data among the two wild-type strains.

In this study, we describe hydroxyectoine overproduction by using recombinant strains of the natural producer C. salexigens genetically engineered (i) to coexpress, in a native-plasmid-based vector, the ectoine and hydroxyectoine genes under the control of the ectA promoter region, (ii) to improve the first approach by increasing the copies of ectD, and (iii) to further improve the two first designs by using an ectoine-deficient mutant as the genetic background. As stated above, transcriptional regulation of the *C*. salexigens ectABC genes for ectoine synthesis is rather complex, with a total of four promoters regulating ectABC transcription (two putative σ^{70} -dependent promoters, one σ^{S} -controlled promoter, and a fourth promoter of unknown specificity) and one putative σ^{32} -dependent promoter driving *ectBC* expression. This multiplicity of promoters allows the cells to respond to many environmental stimuli such as high salinity and temperature and the presence of iron, external osmoprotectants, or the DNA gyrase inhibitor nalidixic acid (13). In H. elongata ATCC 33173^T, Schwibbert et al. (30) found a different but also complex promoter assembly, with two transcriptional initiation sites upstream of *ectA* (corresponding to putative σ^{70} - and σ^{S} -dependent promoters), and a third one mapped immediately upstream of ectC, resembling σ^{54} -controlled promoters. Based on these findings, the authors suggested that ectoine synthesis in H. elongata could be regulated not only by salinity but also by nitrogen supply. In addition, in the presence of the external osmoprotectant betaine, ectoine accumulation is totally abolished in C. salexigens (28) but not in *H. elongata* (24), reflecting an apparently different regulation of ectoine production in both organisms. In summary, with the available data, it is difficult to predict if the same strategy followed in this study would efficiently work in H. elongata.

As stated above, the presence of by-products in any strain devoted to industrial production of hydroxyectoine is undesirable, as it would increase production costs (4). All strains depicted in Table 2 that have been tested for the presence of other solutes show from trace (i.e., *E. coli* DH5 α /pSB01) to moderate (i.e., *H. elongata*, *C. salexigens*, or *P. stutzeri* wild-type strains) amounts of

other contaminating solutes. Therefore, downstream processes involving a certain purification step are mostly unavoidable. For the most promising strain, CHR137/pHYDROX2, hydroxyectoine was the main product, which would be useful to reduce separation and purification costs. In any case, separation of hydroxyectoine from trehalose and glutamate is easy by simple chromatographic techniques (3, 9).

Our findings indicate the superiority of the C. salexigens ectoine-minus strains over the wild-type strain for hydroxyectoine production, including much better yields and specific production rates than the wild type. Production achieved with strain CHR137/pHYDROX2 growing at a relatively low salinity, 4.35% NaCl, exceeds that of most other strains reported elsewhere (Table 2). Its specific hydroxyectoine production yield is of the same order as that of heterologous production by *E. coli* DH5α/pSB01 at 2% NaCl (17), and the absolute yield is much higher. In addition, conversion of ectoine to hydroxyectoine by E. coli/pSB01 was much delayed until late stationary phase, whereas in C. salexigens production was maximal at early stationary phase. Nevertheless, E. coli DH5 α /pSB01 has the advantage of yielding purer hydroxyectoine. In addition, due to its natural ability to cope with strong changes in medium osmolarity, C. salexigens is a much more robust strain than E. coli for the industrial bacterial milking process, and therefore there is much room for improvement of hydroxyectoine production, for instance by continuous fermentation coupled to product extraction by osmotic downshocks. Thus, considering all relevant yield parameters, the C. salexigens recombinant strains are promising candidates for the biotechnological production of hydroxyectoine.

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