

Depósito de investigación de la Universidad de Sevilla

https://idus.us.es/

"This is an Accepted Manuscript of an article published by Elsevier in: INTERNATIONAL JOURNAL OF BIOLOGICAL MACROMOLECULES on 2021, available at: <u>https://doi.org/10.1016/j.ijbiomac.2021.08.043</u>"

1	Rice bran-based bioplastics: effects of the mixing temperature on				
2	starch plastification and final properties.				
3	María Alonso-González ^{1,*} , Manuel Felix ² , Antonio Guerrero ² , Alberto Romero ¹				
4	¹ Departamento de Ingeniería Química, Facultad de Química, Universidad de Sevilla, 41012,				
5	Sevilla, Spain.				
6 7	² Departamento de Ingeniería Química, Escuela Politécnica Superior, Universidad de Sevilla, 41011, Sevilla, Spain.				
8					
9					
10					
11					
12					
13					
14					
15	*MARÍA ALONSO GONZÁLEZ				
16	Departamento de Ingeniería Química				
17	Universidad de Sevilla,				
18	41011, Sevilla (Spain)				
19	E-mail: <u>maralonso@us.es</u>				
20	Phone: +34 635313411				

21 ABSTRACT

22 The agro-food industry produces huge amounts of wastes and by-products with high 23 levels of carbohydrates and proteins, basic food groups that, properly treated, can be 24 employed for the development of bioplastics. These high added-value products represent 25 an alternative to traditional polymers. In this research work, rice bran was mixed with 26 glycerol and water obtaining homogeneous blends which then are processed into 27 bioplastics via injection moulding. The mixing temperature aids starch plastification and 28 thus, affects the properties of the final specimens. In this way, the mechanical 29 characterization revealed improvements for the highest temperature (110 °C) used which, 30 at the same time, exhibited poor physical integrity during water immersion. Although the mechanical properties of the dried system obtained at 80 °C are slightly inferior to those 31 obtained for the non-dried 110 °C system, these specimens are considered more adequate 32 since they exhibited higher physical integrity and, consequently, better operating 33 conditions. 34

35 **Keywords:** bioplastics; starches; injection-moulding.

36 **1. INTRODUCTION**

The annual production of plastics exceeded 368 million metric tons in 2019 [1]. One of the main environmental impacts of plastic production is pollution, caused by its difficult decomposition by microorganisms present in the soil [2]. One possible solution to solve this problem is the production of eco-friendly plastics, that is, bioplastics exhibiting biodegradable capacity. Bioplastics can be generated from two different sources: biodegradable polyesters (petroleum-based), and biopolymers from biodegradable resources [3].

44 Bioplastics formulated with plant proteins are becoming an increasingly popular source of raw materials for bioplastic products, since they are not only biodegradable but are also 45 46 made from renewable resources, such as polysaccharides (i.e., starch), lipids and proteins 47 [4]. Bioplastics from plant proteins have been already developed based on the protein content of plant protein concentrates commercially available, such as rice [5], pea [6], 48 wheat gluten [7], and soy [8] among others. In addition, a large number of studies have 49 50 been carried out using proteins, coming either from plant sources such as zein, wheat gluten or soybean [9–11] or from animal sources such as milk proteins, collagen or gelatin 51 52 [12,13]. For this purpose, they are often mixed with certain plasticizers such as glycerol, sorbitol, water or ethylene glycol [14], to reduce the protein-protein interactions, 53 54 replacing them with protein-plasticizer ones. Thus, the resulting material is suitable for 55 processing by thermomechanical techniques [15]. However, the scientific literature related to the development of bioplastics based on their starch content is scarce except for 56 the research related to thermoplastic starches processed by extrusion [16,17] 57

Starch can be found in different plants, such as wheat, maize, potato and rice [18]. This
material has a granular structure, which consists of two main carbohydrate polymers: the
linear amylose and the highly branched amylopectin. Although starch is in abundance all

over the world, there are not many applications in material science, since the granular structure must be totally destroyed in order to produce thermoplastic starch (TPS), a process called gelatinization. For this purpose, starch is processed under the action of temperature (between 70 and 90 °C), shearing action and water excess. Although water is required, when used on its own it produces brittle products so it is often included with the aid of another plasticizer [19].

67 Proteins and carbohydrates are two basic food groups that can be found in wastes from 68 the rice industry as is the case of rice bran (RB). RB is a residue from brown rice obtained during the rice milling process [20]. Nowadays, this by-product is mostly used for animal 69 70 feeding due to its low price and nutritional richness [21]. Rice is the staple food for more 71 than half of the world's population, and yet by 2030, global rice production must doble 72 to meet the demand [22] thus, emerging technologies that allow the valorization of its by-73 products are highly convenient. The European Commission has granted projects for a 74 "near zero-waste" society such as the NoAW (No Agro-Waste) proposal [23]. In this 75 sense, the development of innovative approaches that allow the conversion of growing 76 agricultural wastes and by-products into eco-efficient bio-based products has been in the spotlight in recent years. In this way, RB could be transformed into high-added-value 77 78 materials after suitable processing, meeting the requirements of circular economy, which 79 aims at enhancing the continuous flow of technical and biological materials while keeping 80 products, components and materials at their highest utility and value and reducing waste to a minimum [24]. 81

This research work aimed to analyse the effect of the mixing temperature during the processing of RB-based bioplastics *via* injection moulding. The temperature employed during the mixing of the raw materials is believed to be a key factor in the properties of the final bioplastics specimens. In order to evaluate the effects of this parameter, different

mixing temperatures will be used characterizing the properties obtained by these means. 86 87 The different temperatures were selected with respect to the gelatinization of starch, which is estimated to happen between 70 and 90 °C. In this way, the authors aim to verify 88 that temperatures around 80 °C will allow starch gelatinization, producing materials 89 90 suitable for injection mounding with proper mechanical and functional properties. In this process, the RB/plasticizer ratio was kept constant, whereas the mixing temperature 91 92 varied from 50 to 110 °C. To evaluate the effects of the different mixing temperatures on 93 the final specimens, the mechanical properties were measured through frequency and 94 temperature sweep tests (rheological characterisation) and tensile tests. Finally, water 95 absorption tests were carried out to evaluate the water uptake capacity and soluble matter 96 loss, whereas SEM microscopy was employed to study the surface morphology of the 97 different specimens.

98 2. EXPERIMENTAL

99 2.1 Materials

100 The rice bran (RB) was provided by Herba Ingredients (San José de la Rinconada, Seville, 101 Spain). The by-product supplied by this company is obtained from the polishing process 102 of the rice variety "vaporized indica white rice". This variety contains for $7.06 \pm 0.09\%$ 103 moisture, $10.50 \pm 0.16\%$ ashes, $13.22 \pm 0.52\%$ proteins, $22.77 \pm 1.33\%$ lipids and 104 approximately 19 and 22 % starch and fibre, respectively (results not published yet). The 105 remaining percentage, i.e., 46.45% of the sample, can be attributed to carbohydrates, 106 according to previous works [25,26]. Water (W) and glycerol (Gly) were employed as 107 plasticizers; the former was deionized-grade water, and the latter was supplied by PANREAC S.A. (Spain). All other reagents were supplied by Sigma Aldrich (USA). 108

109 **2.2. Processing and characterization of blends**

110 2.2.1. *Mixing of blends*

111 To obtain homogeneous blends, sieved RB (< 500 µm) along with water and glycerol 112 were introduced into a HAAKE POLYLAB QC (ThermoScientific, Germany) mixer 113 equipped with counter-rotating rotors. Water is needed in order to break the hydrogen bonds present in starch, which allows its gelatinization, obtaining TPS [15]. In addition, 114 it is well established that, when used on its own, water (W) produces brittle products, thus 115 116 it is often used along with some other plasticizers such as glycerol (Gly) or sorbitol [27], which are also compatible with proteins [8,28,29]. In this research work, different blends 117 containing 55% RB and 45% plasticizer mixture (2:1 W/Gly) were obtained by mixing 118 119 the raw materials for 1 h at 200 rpm, while different mixing temperatures (50, 80, 90 and 120 110 °C) were analysed to evaluate the influence of the mixing temperature used on the plasticization process of RB-based bioplastics. 121

122 2.2.2. Drying of blends

123 In general, the blends mixed at 50, 80, 90 and 110 °C, which can be denoted as M50, 124 M80, M90 and M110, respectively, had to be subjected to drying to lose some of their moisture content. This process was carried out in opened containers at room temperature, 125 126 achieving a final moisture content below 30%. Otherwise, the bioplastics obtained with high moisture-containing blends exhibited voids and cracks that were easily observed, 127 128 probably due to the water excess that evaporated in the mould cavity, as can be seen in 129 Figure S1. It is worth mentioning that the boiling point of glycerol/water solutions is 130 strongly affected by concentration as reported in the literature [30]. Thus, the boiling point of the solution containing 33,3% Gly in water is ca. 103°C, which is clearly exceeded 131 132 inside the mould. During this drying process, they acquired a firmer appearance, which was quantified by the determination of the linear viscoelastic moduli every 24 h until they 133 were ready for injection moulding. Only the blend obtained at 110 °C was suitable for 134

injection right after the mixing stage (M110*) following the processing conditions
mentioned above. This is because moisture was already lower than 30% after mixing at
110°C. In this way, this system was the only one injected as soon as it was homogenised
during the mixing stage.

139 2.2.3. Dynamic Mechanical Thermal Analysis (DMTA) of blends

140 A dynamic mechanical analyser (RSAIII, TA Instruments, USA) was employed in compression mode using a cylindrical geometry (8 mm in diameter) for each blend 141 142 everyday during drying. Strain sweep tests were performed at constant frequency (1 Hz) 143 and temperature to establish the linear viscoelastic region (LVR). Subsequently, the lower 144 critical strain was selected to characterize the viscoelastic modulus at 1 Hz and room 145 temperature. Finally, once the blends remained unchanged, a temperature sweep test was 146 also carried out at 5 °C/min to study the rheological behaviour of the blends between 30 147 and 160 °C. In these measurements, the storage modulus (E'), loss modulus (E'') and loss tangent (tan δ) were determined for the whole temperature range studied. In addition, the 148 149 water content was calculated during the drying process by following the A.O.A.C. 150 methods [31]. In this way, 3 g of sample were placed in a conventional oven (Memmert 151 B216.1126, Germany) at 105 °C for 24 h to calculate the exact water content by mass 152 difference.

For comparison purposes, the M110 blend, was also characterized during drying toevaluate this system processed under the same conditions.

155 2.2.4. Scanning Electron Microscopy (SEM) of blends

Scanning electron microscope (SEM) observations were carried out to determine the importance of the mixing temperature to produce the TPS material. For this purpose, two blends obtained for the same mixing velocity and time, but different mixing temperature (room temperature, M20, and 80 °C, M80) were compared to another blend obtained by milder conditions (M20mc, mixing for 10 min at 50 rpm and room temperature with no added water) trying to observe the starch structure with minimal modifications. The samples were first sputtered with a 10 nm thickness Pd/Au coating using an AC600 Metallizer (Leica, Germany), and then they were observed at 10 kV acceleration voltage and 500x magnification.

165 **2.3 Processing and characterization of bioplastics**

166 2.3.1. Injection moulding

167 Each resulting blend either mixed at 50, 80, 90 or 110 °C after drying (M50, M80, M90 168 or M110) or at 110 °C right after mixing (M110*), was introduced in the cylinder of a 169 Haake pneumatic piston injection moulding equipment (MiniJet II ThermoScientific, Germany) at 50 °C. The temperature of the mould was fixed at 150 °C to favour the 170 171 thermosetting of the specimens according to the results obtained from the temperature sweep tests of the blends and a previous study [32]. Regarding injection and holding 172 pressures, they both were fixed at 500 bar, selecting 15 and 200 s for injection and holding 173 174 time, respectively. By employing these conditions, 60 x 10 x 1 mm rectangular bioplastic specimens, denoted as I50, I80, I90, I110 and I110*, were obtained for subsequent 175 176 characterization.

177 2.3.2. Dynamic Mechanical Thermal Analysis (DMTA) of bioplastics

DMTA tests were carried out with an RSA-III (TA Instruments, USA) on I50, I80, I90, I110 and I110* rectangular specimens using two grips, one at the bottom and one at the top, to study their rheological behaviour in tension mode. Firstly, strain sweep tests were performed to establish the LVR at 1 Hz and room temperature. Then, frequency sweep tests were carried out within the LVR at room temperature from 0.01 to 20 Hz. Finally, temperature sweep tests were also carried out within the LVR at 1 Hz between 30 and
140 °C using a heating rate of 5 °C/min.

185 2.3.3. Tensile tests of bioplastics

Tensile tests were performed with the RSA III (TA Instruments, USA) equipment in continuous deformation mode. Measurements were carried out according to the ISO 527-2:2012 [33], using I50, I80, I90, I110 and I110* rectangular specimens and an extensional rate of 1 mm/min at room temperature. Strain-stress curves were obtained for each sample and three parameters were calculated: maximum tensile strength (σ_{max}), Young's modulus

191 (E) and strain at break (ε_{max}).

192 2.3.4. Water uptake capacity of bioplastics and soluble matter loss

193 The absorption capacity of the bioplastic samples was evaluated by water uptake capacity 194 measurements following the ASTM D570 standard [34]. I50, I80, I90, I110 and I110* rectangular specimens (20 x 10 x 1 mm) were used. According to the standard, the 195 196 samples were subjected to a dehydrothermal treatment in an oven at 50 °C for 24 h to 197 determine the initial dry weight, followed by the weighing of the sample after immersion 198 in distilled water for 24 h. Finally, the specimens were subjected to freeze-drying in a 199 LyoQuest freeze-dryer with a Flask M8 head (Telstar, Spain). Water uptake capacity (WUC) and soluble matter loss (SML) were determinate by Eqs. (1) and (2): 200

201
$$WUC (\%) = \frac{w_2 - w_3}{w_3} \cdot 100$$
 (1)

202
$$SML(\%) = \frac{w_1 - w_3}{w_1} \cdot 100$$
 (2)

Were w_1 , w_2 and w_3 are the weights of the sample after the dehydrothermal treatment, after the immersion step and after the freeze-drying stage, respectively. Samples obtained after freeze-drying were denoted as F50, F80, F90, F110 and F110*, depending on the
initial mixing and drying conditions of the blends used.

207 2.3.5. Scanning Electron Microscopy (SEM) of freeze-dried bioplastic matrices

The microstructure of each final bioplastic after the freeze-drying treatment (F50, F80, F90, F110 or F110*) was observed to determine the influence of the mixing temperature on the structure generated in the bioplastics after water absorption according to the protocol described by Julavittayanukul et al. [35]. The samples were first sputtered with a 10 nm thickness Pd/Au coating using an AC600 Metallizer (Leica, Germany), and then they were observed at 10 kV acceleration voltage and 500x magnification.

214 **2.4 Statistical analyses**

At least three replicates of each measurement were carried out. Statistical analyses were performed using t-test and one-way analysis of variance (ANOVA) (p < 0.05) using the STATGRAPHICS 18 software (Statgraphics Technologies, Inc, NJ, USA). Standard deviations from some selected parameters were calculated. Significant differences are indicated by different letters.

220 **3. RESULTS AND DISCUSSION**

221 **3.1.** Characterization of blends

222 3.1.1. Dynamic Mechanical Thermal Analysis (DMTA) of blends

Two parameters were monitored to evaluate the drying process of the blends obtained after mixing: the elastic modulus at a constant frequency of 1 Hz (E_1 ') and the moisture content (%). Figure 1 shows the evolution of these two parameters over time for the four different blends obtained after mixing at 50, 80, 90 and 110 °C (M50, M80, M90 and M110). As can be seen, the first three blends (M50, M80 and M90) underwent the same evolution, with E_1 ' increasing with time for the first 6-7 days and then remaining

unchanged until the end of its monitoring after 10 days of drying. The values obtained 229 230 show no significant differences, with E₁' being slightly higher for the M80 and M90 231 blends. At the same time, the water content followed the same behaviour as the elastic 232 moduli for the different blends, observing a stabilization after drying for six days. However, its values decreased during the firsts days, from 40 - 45% moisture right after 233 mixing to less than 30% at the end of the experiment, for all the studied systems. At this 234 235 point, the three blends were suitable for injection moulding. Moreover, the relationship 236 between both parameters shows that the elastic modulus increased when the moisture content decreased, which reflects the plasticizer effect of the water contained in the 237 238 sample [36].

239 On the other hand, the M110 blend did not follow such a clear tendency. Right after 240 mixing (day 0), E₁' values were higher than the ones obtained for the other blends and, 241 contrary to the increasing tendency observed before, the values for this system remained 242 practically unchanged. Regarding water content, right after mixing, the moisture content was low, near 20 %, due to the high temperature employed in this process (110 °C). 243 244 However, after 1 day, the M110 blend absorbed some moisture causing the observed fluctuation. It is worth mentioning that, after several attempts, it was found that blends 245 246 were only suitable for injection moulding when the water content was below 30 %, and 247 no successful processing was achieved for higher values. Therefore, the moisture content 248 of the blends was found to be the critical parameter to be evaluated before proceeding with injection moulding. Thus, as mentioned above, excess water (i.e. moisture higher 249 250 than 30%) seems to lead to severe water/glycerol evaporation inside the mould cavity, which is maintained at 150°C, causing the formation of voids and cracks as can be seen 251 in Figure S1. 252

As can be observed in Figure 1, the only blend that can be readily injected after mixing is the one mixed at 110°C, denoted as M110* to distinguish it from the dried blends. This blend was also injected after 10 days of drying as the other systems for comparison purposes, which also ensures that the moisture content was below 30%.

257 Once the blends were stabilized (i.e., 10 days after mixing), temperature sweep tests were 258 carried out between 30 and 160 °C using a heating rate of 5 °C/min. Figure 2 shows the 259 evolution of the elastic and viscous moduli (E' and E'', respectively) with temperature. 260 Although all blends showed a predominantly elastic character, with the elastic modulus being higher than the viscous modulus for the whole range studied, different behaviours 261 262 can be observed when the temperature increased. First, the M80 and M90 blends, show a 263 decrease in E' and E'' with increasing temperature up to 100-120 °C (from 2.6 and 1.5 264 MPa to 1.1 and 0.7 MPa, respectively). Then, both moduli increased again up to 2.0 and 265 1.3 MPa, tending to equilibrate at high temperature. For the whole temperature range, 266 both viscoelastic moduli obtained for the M80 blend are higher than those obtained for 267 M90. On the other hand, the M50 blend followed the same tendency for the first part of 268 the test (between 30 and 100-120 °C). However, above this temperature, the viscoelastic moduli underwent an abrupt decrease accounting for the lowest measured values. Finally, 269 270 the blend mixed at 110 °C was characterized after drying for 10 days (M110), just like the 271 other systems, and right after mixing (M110*). Both blends followed a very similar tendency. At the beginning of the experiment (between 30 and 70 °C), the viscoelastic 272 moduli were higher for the M110* than for M110 (e.g. E' was around 1.0 and 0.6 MPa, 273 274 respectively). Between 70 and 110 °C, both blends followed the same behaviour slightly decreasing with increasing temperature (e.g. from 0.3 to 0.2 MPa). However, both 275 276 systems diverge above 110 °C up to the end of the experiment, being again M110* above M110 for the higher temperatures used (at which E' values drops from 0.09 to 0.04 MPa, 277

respectively). As can be seen, M80 and M90 were the only blends that showed certain
thermosetting potential, with both moduli increasing above 110 °C up to 150°C. For this
reason, and based on the results obtained in previous studies by Alonso-González et al.
[32], 150°C was selected as the temperature of the mould for injection moulding. It can
be assumed that the higher temperatures used hinder the thermosetting potential of the
mixed blends leading to lower viscoelastic moduli for the whole studied range.

The thermosetting potential exhibited by the M80 and M90 samples has been previously observed for pea protein-based blends prepared using a similar procedure at lower temperatures [37]. On the other hand, Felix et al. [38] produced crayfish-based bioplastics from protein/glycerol blends whose viscoelastic moduli upon temperature sweep tests exhibited a decreasing tendency during the whole studied range, thus no thermosetting potential was observed, showing a behaviour similar to that recorded for the two blends mixed at 110 °C.

291 3.1.2. Scanning Electron Microscopy (SEM) of blends

The SEM images revealed that after mixing with mild conditions the M20mc blend still contains some granular starch (Figure 3A). It can be observed that the addition of water while mixing at 200 rpm for 1 h leads to a blend (M20) where the granular structure was partly destroyed (Figure 3B). This structure disappeared completely for the M80 sample (Figure 3C), indicating that the mixing temperature is a key parameter to obtain TPS. Tábi et al. [39] obtained similar SEM images during TPS obtention through extrusion and injection moulding.

299 **3.2. Characterization of bioplastics**

300 3.2.1. Dynamic Mechanical Thermal Analysis (DMTA) of bioplastics

The results obtained for the frequency sweep tests between 0.01 and 20 Hz at room 301 302 temperature are shown in Figure 4 for all the bioplastics injected using either the blends 303 mixed at different temperatures and dried for 10 days (I50, I80, I90 and I110) or with no 304 drying (I110*). The mechanical spectra obtained shows that E' was always higher than E", which indicates that all specimens exhibit a predominantly elastic character [40]. The 305 306 viscoelastic moduli show a moderate frequency dependence, following a power-law 307 tendency to increase with increasing frequency. The power-law exponent ranges from 0.15 for I50 to 0.20 for I110*. This rheological behaviour has been previously observed 308 309 for protein-based bioplastics which exhibited slightly lower power-law exponents from 310 0.15 to 0.18 [41] and from 0.12 to 0.14 [42] for the soy/nanoclay based composites which 311 seems to indicate that the starch content induces stronger frequency dependence. In 312 addition, it should be highlighted that the higher viscoelastic moduli are found for the 313 bioplastics obtained from the blend injected right after mixing, with no drying process, being clearly superior as this system exhibits 180 and 55 MPa for the elastic and viscous 314 moduli, respectively, which are clearly above the second highest one, which would be the 315 316 I90 system, with 68 and 23 MPa for these two parameters. The other four systems showed 317 lower viscoelastic moduli, especially the probe obtained from I110, with E'₁ being ca. 30 318 MPa, and the other three having higher and more similar values (ca. 46 and 60 MPa for 319 150 and 180, respectively). This behaviour could be related to the fact that the system 320 obtained from the blend without drying, was injected with lower moisture content 321 $(\sim 22\%)$, as a result of the higher mixing temperature and no water absorption during 322 drying. This fact involved a lower content of plasticizer which contributed a higher viscoelastic response. However, the lower proportion of water in the plasticizer also led 323 324 to an increase in its boiling point, giving rise to a reduction in the evaporation inside of the mould cavity [30]. The other systems (dried ones) were injected with similar water 325

326 contents (< 30%), and thus showed more similar values. However, the higher 327 temperatures used for the mixing stage led to slightly higher values, indicating the 328 convenience of increasing temperature during starch gelatinization. Regarding the I110 329 bioplastic, the water absorbed during drying did not take place in the gelatinization 330 process, only contributing to hindering the injection moulding stage, leading to poorer 331 results.

332 The systems were also subjected to temperature sweep tests between 30 and 140 °C 333 (Figure 5). In this case, all specimens, except the one obtained from the dried blend mixed at 110 °C (I110), followed the same behaviour, with E' and E'' decreasing with increasing 334 temperature up to 90-100 °C and reaching, at this point, a plateau value, with the 335 336 viscoelastic moduli remaining almost unchanged. In addition, the elastic moduli began 337 clearly differentiated at 30°C, with the I110* system showing the best results (127 and 48 MPa for E' and E'' values, respectively), followed by the I80 and I90 systems, which 338 339 exhibited similar results, with 71 MPa for E' and 23-25 MPa for E'', for the two different systems), with the 50 °C system showing the worst results (E' = 36 MPa and E'' = 10 340 MPa). Although, once the plateau value was reached, they all showed more similar values, 341 342 being the elastic modulus around 13 MPa and the viscous one approximately 3 MPa. 343 Finally, the specimens obtained from the dried blend I110 began with the same tendency, 344 where both moduli decrease with increasing temperature up to 90 °C, with the elastic modulus decreasing from 16 MPa to 6 MPa although, at this point, E' and E'' underwent 345 a more abrupt decrease (about one order of magnitude), and then reached a steady value 346 347 around 120-140 °C, with E' stabilizing at around 0.7 MPa. Again, this differentiated behaviour could be attributed to the fact that this system was the only one absorbing water 348 349 after the mixing stage. Thus, this water did not ease the production of TPS but hindered the injection of the specimens resulting in higher sensitivity to temperature. Similar 350

tendencies can be observed for the same tests performed on defatted rice bran with similar
protein/starch composition processed by extrusion [17] and also with other protein-based
bioplastics [43].

354 *3.2.2. Tensile tests of bioplastics*

Figure 6 shows the stress-strain curves obtained from the tensile tests of all the samples 355 356 evaluated in this work. All systems exhibited a similar behaviour. The system not submitted to drying exhibited the highest stiffness, although it only achieved the second-357 358 lowest elongation at break. The rest of the curves presented much more similar tendencies 359 with varying parameters, with the I80 system showing the higher slope, followed by the I90 system, and finally by the I50 and I110 specimens. Regarding toughness, although 360 361 the I90 specimens presented poorer stiffness than I80 samples, the former exhibited 362 greater elongations, leading to similar areas under the curve and therefore similar 363 toughness. To finish with, the two systems with similar slopes (50 and 110 °C) exhibited 364 quite different elongations, with the system processed at 50 °C being the one with the 365 greatest toughness and the I110 system being the one with the worst tensile properties.

366 Table 1 allows a more accurate evaluation of the three parameters obtained from the stress-strain curves: Young's modulus (E), maximum tensile strength (σ_{max}) and strain at 367 break (ε_{max}). Beginning with the four systems obtained from the dried blends (I50, I80, 368 369 I90 and I110), it can be seen that all parameters improved when the mixing temperature increased from 50 to 80 °C, although further increases had no beneficial effects, especially 370 371 for the system processed at 110 °C, which is in agreement with the previously mentioned 372 detrimental effect for the water absorption during drying. In this way, E increased from 373 10 ± 1 to 33 ± 6 MPa when the temperature of the mixing stage increased from 50 to 80 °C, although lower values (20 ± 1 and 10 ± 1 MPa) were obtained for the I90 and I110 374

375 systems, respectively. Again, σ_{max} reached a maximum value for the I80 system, showing 376 its minimum value for I110 specimens. Finally, ε_{max} also improved from I50 to I80 and 377 I90 systems, being the only parameter that displayed higher values for I90 than for I80 378 bioplastics. The dried system mixed at 110 °C (I110) still showed the lowest value for the 379 final elongation. Similar values have been found for protein [44] and starch-based [17] 380 systems obtained by similar processing techniques.

On the other hand, the system with the highest Young's modulus and tensile strength is the only one that was not subjected to the drying process. The only property that did not improve in this case was the elongation at break, reaching the poorest values $(1.0 \pm 0.1\%)$. The obtained results indicate that higher temperatures during mixing lead to stiffer materials with lower elasticities. This last behaviour is typical of protein-based systems, where E increases with the processing temperature, whereas the elongation at break does not [8].

388 *3.2.3.* Water uptake capacity of bioplastics and soluble matter loss

Figure 7A shows the water uptake capacity values for the different bioplastics obtained. The highest values are those obtained for the systems mixed at the highest temperature, either with the dried (I110) or non-dried systems (I110*), achieving $234 \pm 21\%$, and $252 \pm 75\%$, respectively. The other three systems (I50, I80 and I90) exhibited lower absorption capacities, not showing any significant difference among them. These values of water uptake capacity are between those typically obtained by hydrophilic proteinbased bioplastics [37,45,46] and those shown by starch-based specimens [47,48].

High water uptake capacities correspond to high soluble matter losses, as can be seen in Figure 7B. In this way, the systems which underwent the highest losses were the two obtained from the blends mixed at 110 °C, being 37 ± 7 and $37 \pm 16\%$ for the dried (I110)

and non-dried (I110*) systems, respectively. In addition, these two systems did not 399 400 maintain their integrity during water immersion, appearing fissures in the specimens, 401 which resulted in higher specific surfaces and, thus, higher water uptake capacity values. 402 The appearance of the fissured specimens can be seen in Figure S2. On the other hand, the I50, I80 and I90 systems exhibited lower values, especially the last one with $25 \pm 1\%$. 403 The other two specimens (I50 and I80) obtained SML values of $31.6 \pm 0.3\%$ and $27 \pm$ 404 405 1%, respectively. This result is also in line with the ones reported in the aforementioned 406 study [43].

407 These results reveal the importance of selecting a proper mixing temperature. When the temperature was fixed to 50 °C, the gelatinization of starch is not achieved, leaving a 408 409 partial granular structure with poorer processability. Although the physical integrity is 410 not compromised, the inferior mechanical properties evidence this fact. However, 411 temperatures of 80 and 90 °C allow complete gelatinization during mixing, providing a 412 material suitable for injection moulding that undergoes retrogradation and some 413 thermosetting phenomenon in the case of the protein fraction, resulting in specimens with both good mechanical performance and physical integrity. Finally, the poorer physical 414 integrity provided by the higher temperature used could be because water is already lost 415 during mixing at 110 °C, leading to an early starch retrogradation even before injection, 416 417 being the bioplastic sample entirely formed through protein-related events. Regarding the lipid and fibre fractions, no significant effects are expected during the bioplastics 418 419 processing since rice bran does not undergo any changes before 150 °C in thermal analysis 420 [26]. However, certain fibre concentrations might have a reinforcing effect upon final 421 properties [49].

422

3.2.4. Scanning Electron Microscopy (SEM) of freeze-dried bioplastic matrices

Figure 8 shows the SEM micrographs of the different bioplastics obtained after the freeze-423 424 drying stage. As can be seen, the observed morphologies match the results obtained 425 before, especially regarding functional properties, in such a way that greater surface homogeneities can be associated with higher WUC, improving from samples F50 and 426 427 F80 (micrographs A and B) to samples F110 and F110* (micrographs C and D). It can be assumed that this higher temperature led to fewer voids and fissures, and thus a more 428 429 homogeneous distribution of the active matter, which translates into higher absorption 430 capacities. The obtained micrographs are similar to those obtained by Tábi et al. [39] and Ferreira et al. [50] for starch-based samples processed using water as the plasticizer. 431

432 4. CONCLUSIONS

The selected conditions, compatible with both proteins and starches, led to the successful 433 development of RB-based bioplastics by injection moulding. The mixing stage, the one 434 435 including the parameter under study, produced different blends that showed rheological differences during and after drying. Those differences made one of them (the M110* 436 system) suitable for injection moulding right after mixing while the rest of them had to 437 438 undergo an drying stage in order to lose some water before being subjected to injection 439 moulding. It was concluded that, under the experimental conditions selected for the injection moulding process, moisture of blends had to achieve a content lower than 30% 440 441 to obtain proper specimens. This limitation may be explained in terms of a reduction in 442 the boiling point of the Gly/W solution with increasing water that may induce excessive evaporation from inside the mould cavity. 443

The mechanical characterization carried out on the bioplastic samples revealed two superior specimens in terms of rheological and tensile parameters: the system processed at 110 °C without drying (I110*) and the dried system mixed at 80 °C (I80). When water uptake capacity was measured, the two systems mixed at the highest temperature (I110 and I110^{*}) exhibited clearly improved values compared to the others, although they exhibited much poorer physical integrities, which could be due to their high soluble matter losses and the fact that they started to lose integral consistency upon water immersion. These two differentiated behaviours could be associated with different morphologies observed in the SEM micrographs, where the more homogeneous surfaces correspond to the systems processed at higher temperatures (110 °C) leading to a more successful injection-moulding processed and a greater distribution of the active matter.

This work evidences the possibility of manufacturing bioplastics from RB, as well as the 455 effect of water as a plasticizer, which, on the one hand, is required during the mixing 456 457 stage, and, on the other hand, determines the final mechanical and functional properties, based on its content. A proper mixing temperature (i.e., 80 °C) is required to produce 458 suitable bioplastics with balanced properties. Furthermore, the measured properties seem 459 to be convenient for those applications that require materials exhibiting high water 460 461 absorption behaviour and still require suitable end-use mechanical properties, ensuring 462 their physical integrity. This should be the case of biodegradable water absorption 463 materials for healthcare, agriculture or horticulture applications. In addition, the study of water uptake capacity in bioplastic systems is receiving increasing attention recently 464 465 because of their important applications in the fields of biomedical, pharmaceutical, environmental and agricultural engineering. 466

467 ACKNOWLEDGEMENTS

The authors acknowledge the University of Seville for the VPPI-US grant (Ref.-II.5) to Manuel Felix, and the financial support of the project RTI2018-097100-B-C21 (MCI/AEI/FEDER, UE) which supported this study. The authors also thank CITIUS for granting access to and their assistance with the Microscopy service. The authors also kindly thank Herba Ingredients for providing the raw material used in this study.

473 **REFERENCES**

- [1] M. Garside, Global plastic production 1950-2019 | Statista, STATISTA. (2020). 474 475 https://www.statista.com/statistics/282732/global-production-of-plastics-since-476 1950/ (accessed January 28, 2021). 477 [2] Y. Yan, Y. Ren, X. Li, X. Zhang, H. Guo, Y. Han, J. Hu, A polysaccharide from green tea (Camellia sinensis L.) protects human retinal endothelial cells against 478 479 hydrogen peroxide-induced oxidative injury and apoptosis, Int. J. Biol. Macromol. 115 (2018) 600–607. https://doi.org/10.1016/j.ijbiomac.2018.04.011. 480 L. Avérous, Biodegradable multiphase systems based on plasticized starch: A 481 [3]
- review, J. Macromol. Sci. Polym. Rev. (2004). https://doi.org/10.1081/MC200029326.
- 484 [4] B.P. Mooney, The second green revolution? Production of plant-based
 485 biodegradable plastics, Biochem. J. 418 (2009) 219–232.
- 486 https://doi.org/10.1042/BJ20081769.
- 487 [5] M. Félix, A. Lucio-Villegas, A. Romero, A. Guerrero, Development of rice
 488 protein bio-based plastic materials processed by injection molding, Ind. Crops
 489 Prod. 79 (2016) 152–159. https://doi.org/10.1016/j.indcrop.2015.11.028.
- 490 [6] V. Perez-Puyana, M. Felix, A. Romero, A. Guerrero, Effect of the injection
- 491 moulding processing conditions on the development of pea protein-based
- 492 bioplastics, J. Appl. Polym. Sci. 133 (2016) n/a-n/a.
- 493 https://doi.org/10.1002/app.43306.
- 494 [7] M. Jiménez-Rosado, L.S. Zarate-Ramírez, A. Romero, C. Bengoechea, P. Partal,
 495 A. Guerrero, Bioplastics based on wheat gluten processed by extrusion, J. Clean.

496		Prod. (2019). https://doi.org/10.1016/j.jclepro.2019.117994.				
497	[8]	L. Fernández-Espada, C. Bengoechea, F. Cordobés, A. Guerrero, Protein/glycerol				
498		blends and injection-molded bioplastic matrices: Soybean versus egg albumen, J.				
499		Appl. Polym. Sci. 133 (2016) 43524. https://doi.org/10.1002/app.42980.				
500	[9]	B. Ghanbarzadeh, A.R. Oromiehie, M. Musavi, Z.E. D-Jomeh, E.R. Rad, J.				
501		Milani, Effect of plasticizing sugars on rheological and thermal properties of zein				
502		resins and mechanical properties of zein films, Food Res. Int. (2006).				
503		https://doi.org/10.1016/j.foodres.2006.05.011.				
504	[10]	L.S. Zárate-Ramírez, A. Romero, I. Martínez, C. Bengoechea, P. Partal, A.				
505		Guerrero, Effect of aldehydes on thermomechanical properties of gluten-based				
506		bioplastics, Food Bioprod. Process. (2014).				
507		https://doi.org/10.1016/j.fbp.2013.07.007.				
508	[11]	M. Yamada, S. Morimitsu, E. Hosono, T. Yamada, Preparation of bioplastic				
509		using soy protein, Int. J. Biol. Macromol. 149 (2020) 1077-1083.				
510		https://doi.org/https://doi.org/10.1016/j.ijbiomac.2020.02.025.				
511	[12]	B. Cuq, N. Gontard, S. Guilbert, Proteins as agricultural polymers for packaging				
512		production, Cereal Chem. 75 (1998) 1–9.				
513		https://doi.org/10.1094/cchem.1998.75.1.1.				
514	[13]	V. Perez-Puyana, M. Felix, L. Cabrera, A. Romero, A. Guerrero, Development of				
515		gelatin/chitosan membranes with controlled microstructure by electrospinning,				
516		Iran. Polym. J. 28 (2019) 921–931. https://doi.org/10.1007/s13726-019-00755-x.				
517	[14]	J.M. Aguilar, C. Bengoechea, E. Pérez, A. Guerrero, Effect of different polyols				
518		as plasticizers in soy based bioplastics, Ind. Crops Prod. 153 (2020) 112522.				

- 519 https://doi.org/10.1016/j.indcrop.2020.112522.
- 520 [15] T. Mekonnen, P. Mussone, H. Khalil, D. Bressler, Progress in bio-based plastics
 521 and plasticizing modifications, J. Mater. Chem. A. 1 (2013) 13379–13398.
 522 https://doi.org/10.1039/c3ta12555f.
- 523 [16] M. Vikman, M. Itävaara, K. Poutanen, Measurement of the biodegradation of
- starch-based materials by enzymatic methods and composting, J. Environ. Polym.
 Degrad. (1995). https://doi.org/10.1007/BF02067790.
- 526 [17] Y. Klanwan, T. Kunanopparat, P. Menut, S. Siriwattanayotin, Valorization of
- 527 industrial by-products through bioplastic production: Defatted rice bran and kraft
- 528 lignin utilization, J. Polym. Eng. 36 (2016) 529–536.
- 529 https://doi.org/10.1515/polyeng-2015-0301.
- 530 [18] R. Thakur, P. Pristijono, C.J. Scarlett, M. Bowyer, S.P. Singh, Q. V. Vuong,

531 Starch-based films: Major factors affecting their properties, Int. J. Biol.

- 532 Macromol. 132 (2019) 1079–1089.
- 533 https://doi.org/10.1016/j.ijbiomac.2019.03.190.
- 534 [19] R.F.T. Stepto, Understanding the processing of thermoplastic starch, in:
- 535 Macromol. Symp., 2006. https://doi.org/10.1002/masy.200651382.
- 536 [20] I. Sereewatthanawut, S. Prapintip, K. Watchiraruji, M. Goto, M. Sasaki, A.
- 537 Shotipruk, Extraction of protein and amino acids from deoiled rice bran by
- subcritical water hydrolysis, Bioresour. Technol. 99 (2008) 555–561.
- 539 https://doi.org/10.1016/j.biortech.2006.12.030.
- 540 [21] G.K. Chandi, D.S. Sogi, Functional properties of rice bran protein concentrates,
- 541 J. Food Eng. 79 (2007) 592–597. https://doi.org/10.1016/j.jfoodeng.2006.02.018.

542	[22]	M.S. Turmel, B.L. Turner, J.K. Whalen, Soil fertility and the yield response to			
543		the System of Rice Intensification, Renew. Agric. Food Syst. 26 (2011) 185-192.			
544		https://doi.org/10.1017/S174217051100007X.			
545	[23]	L. Caudet, V. von Hammerstein-Gesmold, A new bioeconomy strategy for a			
546		sustainable Europe, Eur. Comm. Press Release. (2018).			
547	[24]	Ellen MacArthur Foundation and McKinsey Center for Business and			
548		Environment, Growth within: a circular economy vision for a competitive			
549		europe, 2015.			
550	[25]	Siswanti, R.B.K. Anandito, E. Nurhartadi, B.D. Iskandar, Effect of various heat			
551		treatment on physical and chemical characteristics of red rice bran (Oryza nivara			
552		L.) Rojolele, IOP Conf. Ser. Mater. Sci. Eng. 633 (2019) 012046.			
553		https://doi.org/10.1088/1757-899X/633/1/012046.			
554	[26]	T. Kunanopparat, P. Menut, W. Srichumpoung, S. Siriwattanayotin,			
555		Characterization of Defatted Rice Bran Properties for Biocomposite Production,			

- J. Polym. Environ. 22 (2014) 559–568. https://doi.org/10.1007/s10924-014-0683-
- 557

6.

- 558 [27] P.M. Forssell, J.M. Mikkilä, G.K. Moates, R. Parker, Phase and glass transition
- behaviour of concentrated barley starch-glycerol-water mixtures, a model for
- thermoplastic starch, Carbohydr. Polym. 34 (1997) 275–282.
- 561 https://doi.org/10.1016/s0144-8617(97)00133-1.
- 562 [28] A. Redl, M.H. Morel, J. Bonicel, S. Guilbert, B. Vergnes, Rheological properties
 563 of gluten plasticized with glycerol: dependence on temperature, glycerol content
- and mixing conditions, Rheol. Acta. 38 (1999) 311–320.
- 565 https://doi.org/10.1007/s003970050183.

- V.M. Hernandez-Izquierdo, J.M. Krochta, Thermoplastic processing of proteins
 for film formation A review, J. Food Sci. (2008). https://doi.org/10.1111/j.17503841.2007.00636.x.
- 569 [30] G.P. Association, Physical properties of glycerine and its solutions, 1963.
- 570 [31] AOAC, Official Methods of Analysis of AOAC International, 2005.
- 571 [32] A.R. M. Alonso-González, M. Felix, A. Guerrero, Effects of Mould Temperature
 572 on Rice Bran-Based Bioplastics Obtained by Injection Moulding, 13 (2021) 398.
 573 https://doi.org/10.3390/polym13030398.
- 574 [33] International Organization for Standardization, ISO 527-1:2012 Plastics --
- 575 Determination of tensile properties -- Part 1: General principles, Geneva. (2012).
- 576 [34] D570, ASTM D 570 98 Standard Test Method for Water Absorption of

577 Plastics, ASTM Stand. (1985). https://doi.org/10.1520/D0570-98.

- 578 [35] O. Julavittayanukul, S. Benjakul, W. Visessanguan, Effect of phosphate
- 579 compounds on gel-forming ability of surimi from bigeye snapper (Priacanthus
- tayenus), Food Hydrocoll. (2006). https://doi.org/10.1016/j.foodhyd.2005.12.007.
- J. Irissin-Mangata, G. Bauduin, B. Boutevin, N. Gontard, New plasticizers for
 wheat gluten films, Eur. Polym. J. 37 (2001) 1533–1541.
- 583 https://doi.org/10.1016/s0014-3057(01)00039-8.
- [37] V. Perez, M. Felix, A. Romero, A. Guerrero, Characterization of pea proteinbased bioplastics processed by injection moulding, Food Bioprod. Process. 97
 (2016) 100–108. https://doi.org/10.1016/j.fbp.2015.12.004.
- 587 [38] M. Felix, A. Romero, F. Cordobes, A. Guerrero, Development of crayfish bio588 based plastic materials processed by small-scale injection moulding, J. Sci. Food

- 589 Agric. 95 (2015) 679–687. https://doi.org/10.1002/jsfa.6747.
- 590 [39] T. Tábi, J.G. Kovács, Examination of injection moulded thermoplastic maize
- starch, Express Polym. Lett. 1 (2007) 804–809.
- 592 https://doi.org/10.3144/expresspolymlett.2007.111.
- 593 [40] H.A. Barnes, A Handbook of Elementary Rheology, University of Wales,

594 Institute of Non-Newtonian Fluid Mechanics, Wales, 2000.

- 595 [41] V. Bourny, V. Perez-Puyana, M. Felix, A. Romero, A. Guerrero, Evaluation of
- the injection moulding conditions in soy/nanoclay based composites, Eur. Polym.
- 597 J. 95 (2017) 539–546.
- 598 https://doi.org/https://doi.org/10.1016/j.eurpolymj.2017.08.036.
- 599 [42] M. Felix, I. Martinez, A. Romero, P. Partal, A. Guerrero, Effect of pH and
- 600 nanoclay content on the morphology and physicochemical properties of soy
- protein/montmorillonite nanocomposite obtained by extrusion, Compos. Part B
 Eng. 140 (2018) 197–203.
- 603 https://doi.org/https://doi.org/10.1016/j.compositesb.2017.12.040.
- 604 [43] V. Perez, M. Felix, A. Romero, A. Guerrero, Characterization of pea protein-

based bioplastics processed by injection moulding, Food Bioprod. Process. 97
(2016) 100–108. https://doi.org/10.1016/j.fbp.2015.12.004.

- 607 [44] M. Felix, V. Perez-Puyana, A. Romero, A. Guerrero, Production and
- 608 Characterization of Bioplastics Obtained by Injection Moulding of Various
- 609 Protein Systems, J. Polym. Environ. 25 (2017) 91–100.
- 610 https://doi.org/10.1007/s10924-016-0790-7.
- 611 [45] L. Fernández-Espada, C. Bengoechea, F. Cordobés, A. Guerrero,

- Thermomechanical properties and water uptake capacity of soy protein-based
 bioplastics processed by injection molding, J. Appl. Polym. Sci. 133 (2016)
 43524. https://doi.org/10.1002/app.43524.
- 615 [46] E. Álvarez-Castillo, A. Del Toro, J.M. Aguilar, A. Guerrero, C. Bengoechea,
- 616 Optimization of a thermal process for the production of superabsorbent materials
- based on a soy protein isolate, Ind. Crops Prod. 125 (2018) 573–581.
- 618 https://doi.org/10.1016/j.indcrop.2018.09.051.
- 619 [47] J. Yang, Y.C. Ching, C.H. Chuah, N.S. Liou, Preparation and characterization of
- 621 oils, Polymers (Basel). 13 (2021) 1–15. https://doi.org/10.3390/polym13010094.

starch/empty fruit bunch-based bioplastic composites reinforced with epoxidized

- 622 [48] S.W. Lusiana, D. Putri, I.Z. Nurazizah, Bahruddin, Bioplastic Properties of Sago-
- 623 PVA Starch with Glycerol and Sorbitol Plasticizers, J. Phys. Conf. Ser. 1351

624 (2019) 0–8. https://doi.org/10.1088/1742-6596/1351/1/012102.

- 625 [49] S. Gamero, M. Jiménez-Rosado, A. Romero, C. Bengoechea, A. Guerrero,
- 626 Reinforcement of Soy Protein-Based Bioplastics Through Addition of
- 627 Lignocellulose and Injection Molding Processing Conditions, J. Polym. Environ.
- 628 2019 276. 27 (2019) 1285–1293. https://doi.org/10.1007/S10924-019-01430-1.
- 629 [50] W.H. Ferreira, M.M.I.B. Carmo, A.L.N. Silva, C.T. Andrade, Effect of structure
- and viscosity of the components on some properties of starch-rich hybrid blends,
 Carbohydr. Polym. 117 (2015) 988–995.
- 632 https://doi.org/10.1016/j.carbpol.2014.10.018.

633

634 FIGURE CAPTIONS

Figure 1: Fit of the elastic modulus at 1 Hz (E_1 ') and moisture content over drying time

of the M50, M80, M90 and M110 blends. The injectability limit (i.e. the maximum

637 moisture content below which the blends can be injected) is also shown.

- **Figure 2:** Temperature sweep tests at 5°C/min between 30 and 160 °C for the blends
- obtained after mixing at different temperatures and drying for 10 days (M50, M80, M90
- and M110) or mixed at 110 °C with no drying (M110*).
- Figure 3. SEM micrographs of the blends obtained by mixing (A) at 50 rpm for 10 min,
 room temperature and no added water (M20mc) (B) at 200 rpm for 1h and room
 temperature (M20) and (C) at 200 rpm for 1h and 80 °C (M80).
- **Figure 4.** Frequency sweep tests between 0.01 and 20 Hz for the bioplastics obtained from the different blends after drying for 10 days (I50, I80, I90 and I110) and with no drying (I110*).
- Figure 5. Temperature sweep tests at 5°C/min between 30 and 140 °C for the bioplastics
 obtained from the different blends after drying for 10 days (I50, I80, I90 and I110) and
 with no drying (I110*).
- Figure 6. Stress-strain curves from the tensile tests performed on the bioplastic samples
 obtained from the different blends (I50, I80, I90 and I110) and with no drying (I110*).
- Figure 7. (A) Water uptake capacity (WUC) and (B) soluble matter loss (SML) of the
 bioplastic samples obtained from the different blends: mixed at 50, 80, 90 and 110 °C
 after drying and mixed at 110 °C with no drying (110 °C*).
- Figure 8. SEM micrographs of the bioplastic samples obtained after freeze-drying of
 bioplastics processed from different blends (A) F50, (B) F80, (C) F110 and (D) F110*.

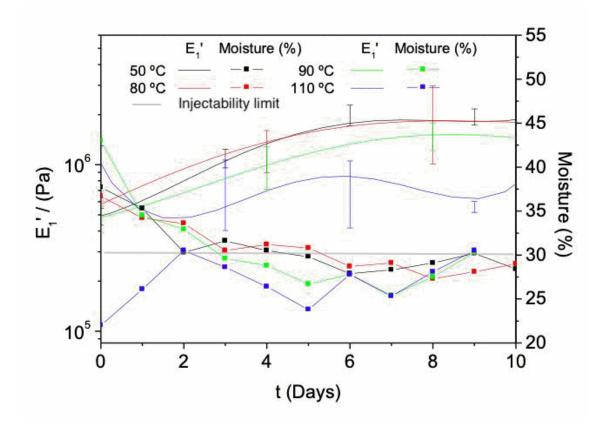


Figure 1.

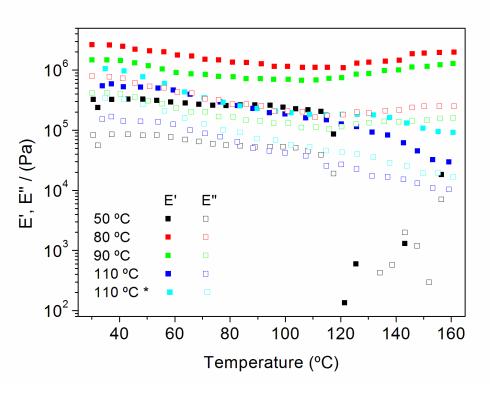


Figure 2

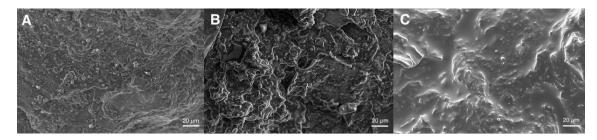


Figure 3

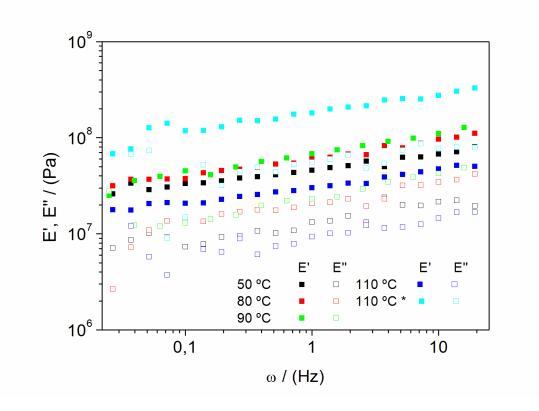


Figure 4

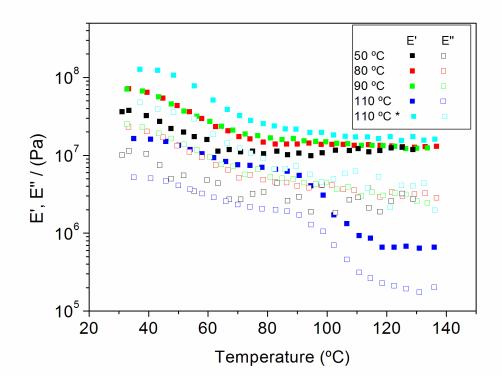


Figure 5

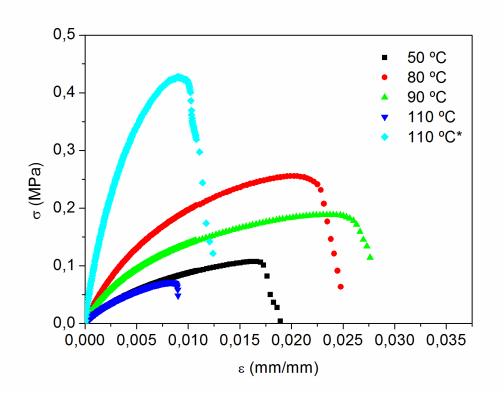


Figure 6

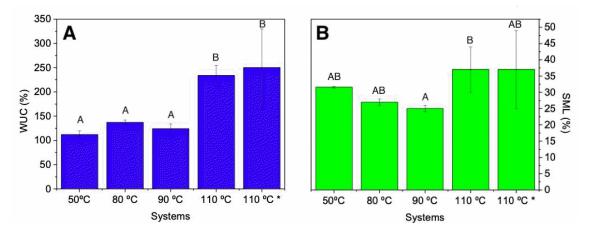


Figure 7

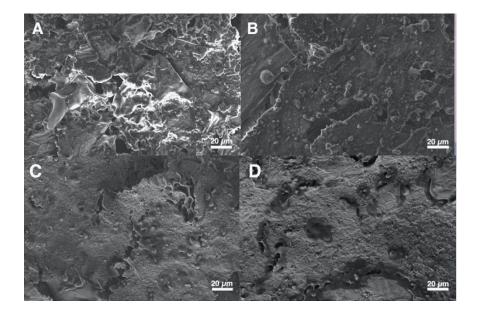


Figure 8

TABLE CAPTIONS

Table 1: Young's modulus, maximum tensile strength and Elongation at break of the different processed systems. Different letters within a column indicate significant differences (p<0.05).

System	E (MPa)	σ_{max} (MPa)	ϵ_{max} (%)
<i>I50</i>	10 ± 1^{A}	0.12 ± 0.01^{A}	$1.9\pm0.2^{\rm BC}$
I80	$33 \pm 6^{\text{C}}$	$0.27\pm0.01^{\rm B}$	$2.4\pm0.3^{\rm C}$
<i>I90</i>	20 ± 1^{B}	$0.19 \pm 0.01^{\circ}$	$2.5 \pm 0.5^{\mathrm{C}}$
<i>I110</i>	10 ± 1^{A}	$0.073\pm0.006^{\mathrm{D}}$	$1.4\pm0.5^{\rm B}$
<i>I110</i> *	80 ± 1^{D}	$0.43 \pm 0.04^{\mathrm{E}}$	$1.0 \pm 0.1^{\mathrm{A}}$