1 Influence of the welan gum biopolymer concentration on the rheological pr	operties,
---	-----------

2 droplet size distribution and physical stability of thyme oil/W emulsions

3 M. José Martin-Piñero, M. Carmen García, José Muñoz, Maria-Carmen Alfaro-

4 Rodriguez\*

5 Departamento de Ingeniería Química. Facultad de Química. Universidad de Sevilla. C/

6 Profesor García González, s/n. 41012 Sevilla. Spain

7 \* Corresponding author

8 e-mail: alfaro@us.es

9 Tel: +34 954 55 64 47

10 Fax: +34 954 55 64 41

### 11 Abstract.

The objective of this work is to obtain a stable and natural antimicrobial delivery system. 12 Thus, the effect of the addition of a natural polysaccharide such as welan gum on the 13 14 linear viscoelastic properties, flow behaviour, droplet size distribution and physical 15 stability of thyme oil/W emulsions formulated with a wheat-derived surfactant was studied. All emulsions obtained show submicron diameters regardless of the 16 17 concentration of welan. Emulsion without gum shows Newtonian behaviour under steady shear. Meanwhile, emulsions containing welan gum show a weak gel-like behaviour with 18 higher G' and G" values on increasing the content of gum in the emulsion. Their flow 19 20 curves illustrate a shear thinning behaviour with much greater viscosity than that exhibited by emulsions without gum. This behaviour fits well to the Cross model. The 21 main destabilization process of thyme oil/W emulsion without gum is creaming versus 22

flocculation and coalescence in emulsions containing welan. Rheology, diffraction laser and multiple light scattering techniques have proved that welan gum is an important rheological modifier for thyme oil/W ecological emulsions, it being possible to control the rheological properties of these emulsions by adjusting the concentration of gum. However, welan gum does not improve the physical stability of these emulsions.

28 Keywords: Welan gum, Thyme oil, Emulsions, Rheology, Physical stability.

#### 29 **1.- Introduction.**

Nowadays, many industries are looking for new ecofriendly and sustainable products,
which can be used in different applications. Ecological emulsions are one of these
products. Finding the right formulation which fulfils environmental and non-toxicity
requirements is essential for researchers within both the research and industrial fields.

As far as formulations are concerned, one of the most important ingredients in emulsions 34 35 is the surfactant. Surfactants are amphiphilic molecules formed by a polar head and a lipophilic tail which can be grouped by the charge of their polar head groups: cationic, 36 37 anionic, amphoteric (zwitterionic) or non-ionic. In addition, surfactants can also be 38 classified by their hydrophilic lipophilic balance (HLB) value. The range of HLB values 39 is from 0 to 20. HLB <9 refers to lipophilic surfactants and HLB> 11 to hydrophilic. Therefore, generally for emulsions of type O / W the emulsifiers have an HLB between 40 41 8 and 18 and for W / O emulsions of 3-8 [1]. It should be noted that the use of emulsifiers whose hydrophilic lipophilic balance (HLB) value is close to the required HLB for oil 42 43 could enable the formulation of stable emulsions. In this work, a non-ionic surfactant, specifically the alkyl poly pentoside commercially known as Appyclean 6548 (D-44 xylofuranose, oligomeric tetradecyl and octodecyl glycoside, C14, C18 alcohol) is used. 45 46 This surfactant possesses an HLB value of 9.25 which has been shown to be the optimum HLB value necessary to obtain stable thyme essential oil emulsions [2]. Appyclean 6548
is a newly-developed surfactant derived from renewable raw materials such as wheat
biomass. The alkyl poly pentoside surfactants are made of pentosides derived from
hemicellulose [3], which is not digestible by human intestinal digestive enzymes.
However, this kind of food fiber could be utilized by members of the intestinal microbial
microbiota like a prebiotic product.[4]. In addition, this surfactant fulfils the requirements
to be used in ecolabel formulations.

In this work, thyme essential oil is used as oil phase. This essential oil is classified as a 54 55 GRAS product by the United States Food and Drug Administration [5]. Thyme Vulgaris, has very high antioxidant activity due to its main components: thymol, carvacrol,  $\gamma$ -56 57 terpinene, myrcene, linalool, p- cymene, limonene, 1,8-cineole, and α-pinene. Among other essential oils, thyme oil has relatively strong antimicrobial activity which it makes 58 it suitable for use in the food field [6,7], Thyme oil is found to be effective against 59 Salmonella typhimurium L. monocytogenes, A. hydrophila and autochthonous flora 60 spoilage in meat products [8]. Nevertheless, thyme essential oil emulsions might undergo 61 62 one or several destabilization mechanisms, such as flocculation, coalescence, Ostwald 63 ripening or creaming. The incorporation of biopolymers into the continuous phase of emulsions decreases or prevents the movement of droplets and increases the viscosity of 64 65 the continuous phase, reducing the creaming destabilization process. The use of natural polysaccharides in food or cosmetic applications as thickening, stabilizing and 66 emulsifying agents is due to their biocompatibility, biodegradability and non-toxicity. In 67 this study, welan gum is used as a polysaccharide in order to enhance the rheological 68 properties of emulsions. 69

Welan is an anionic extracellular polysaccharide, secreted by the micro-organism 70 71 Sphingomonas sp., namely from Alcaligenes sp., ATCC 31555, a gram negative microorganism. It is used in a wide variety of applications in several fields such as food, 72 coating materials, medicine and the petroleum and cement industries [9]. Specifically, 73 this gum can be used as an ingredient in food products like jellies, beverages or dairy 74 products in which it can act as a thickening, suspending, binding, emulsifying, stabilizing 75 76 and viscosifying agent [10]. Structurally, it is composed of 1-mannose, 1-rhamnose, dglucose, and d-glucuronic acid.[11]. The chemical structure is essential in order to explain 77 the behaviour in aqueous phase. For example, although gellan, welan or rhamsan, all of 78 79 which are derived from Sphingomonas sp, are structurally close, they have different behaviours in different mediums. Thus, while gellan can make stable gels in the presence 80 of salts, rhamsan and welan give only weak gels or very viscous solutions with a high 81 82 degree of thermal, pH and salinity stability [12].

Despite the advantages of this environmentally friendly polysaccharide, there are only a
few studies dealing with the use of welan gum in oil-in-water emulsions. In addition, there
have been no previous studies concerning the physical stability and rheological behaviour
of thyme essential oil emulsions prepared with welan gum.

In this study, we investigate the influence of welan gum concentration to improve the rheological properties of emulsions using thyme essential oil as dispersed phase. Additionally, the effect on the physical stability of emulsions is studied. All the components selected to formulate the emulsions are environmentally friendly materials (thyme essential oil, welan and appyclean 6548). The combination of rheology, laser diffraction and multiple light scattering techniques demonstrated that these results have 93 important implications for the design and utilisation of emulsions as antimicrobial94 delivery systems in the food industry.

#### 95 **2.-Materials and Methods.**

96 *2.1. Materials.* 

97 Thyme essential oil (938 g/l), supplied by Bordas Chinchurreta S.A, and a wheat-derived
98 surfactant called Appyclean 6548 obtained from Wheatoleo are used as oil phase and
99 emulsifier respectively. Sodium azide (0.1wt%) is used to avoid microbiological
100 contamination. Welan gum (K1A96) is used as supplied by CP Kelco Company (San
101 Diego, USA).

102 2.2. Emulsification Procedure.

The continuous phases are prepared by dissolving 0.1 wt% sodium azide in ultrapure 103 104 water cleansed using a Milli-Q water purification system. The emulsifier, Appyclean 6548 (6wt%) is melted and dissolved in the dispersed phase (thyme oil -40wt%) due to 105 the fact that it is solid and immiscible in water. The mixture of oil and surfactant is heated 106 107 to 70°C for 30 minutes and then cooled to 25°C. Once at this temperature, a total mass of 200 g of the coarse emulsions is prepared in two steps using a rotor-stator device equipped 108 109 with a mesh screen (Silverson L5M) at 2000 rpm. Firstly, the mixture of solvent and surfactant is gradually added for 180s to the aqueous phase. Subsequently, a batchwise 110 procedure is carried out for 30s. High pressure homogenization is carried out with a 111 112 microfluidization system (M110P with an F12Y interaction chamber, Microfluidics, USA) at 2500psi. Coarse emulsions are passed once through the microfluidization 113 114 system.

Finally, the gum is added very slowly to the final emulsions. The emulsions are
mechanically stirred using an Ika-Visc MR-D1 (Ika, Germany), for two hours at 500rpm.
Five emulsions are prepared using different gum concentrations (0, 0.05, 0.1, 0.15, 0.2
wt%). Two replicates of each emulsion with a final weight of 200g are prepared.

119 2.3. *Rheological properties.* 

The rheological characterization involved stress and frequency sweeps in small amplitude 120 121 oscillatory shear experiments (SAOS) and stepwise steady shear flow tests. Haake-122 MARS controlled-stress rheometer (Thermo-Scientific, Germany) is used to carry out the 123 rheological experiments. Flow curves are performed using a 60/1° double cone geometry for emulsions without gums. Emulsions with gums are measured using a serrated plate-124 plate sensor (60 mm). Flow curves are carried out in a range of 0.05 to 19 Pa. Stress 125 126 sweeps are performed in a range of 0.05 to 19 Pa at 1 Hz. Equilibration time prior to rheological tests is 300s. All measurements are performed at 25 °C  $\pm$  0.1 °C using a C5P 127 128 Phoenix circulator (Thermo) and in duplicate, the values shown being the average of the two replicates. 129

### 130 Microscopy

An optical microscope Axio Scope A1 (Carl Zeiss) with a 40x objective is used to observethe microstructure of the emulsions at room temperature.

133 *2.4. Droplets size distribution measurements.* 

134 Size distribution of oil droplets is determined by the laser diffraction technique

135 (Mastersizer 2000, Malvern, Worcestershire, United Kingdom). Sauter diameter (D3,2),

volume-weighted mean diameter (D4, 3) and span are the parameters selected to discuss

the results. D3,2 and D4,3 values are obtained from the following equation:

138 
$$D_{3,2} = \frac{\sum_{i=1}^{N} n_i d_i^3}{\sum_{i=1}^{N} n_i d_i^2}$$
 (Eq. 1)  $D_{4,3} = \frac{\sum_{i=1}^{N} n_i d_i^4}{\sum_{i=1}^{N} n_i d_i^3}$  (Eq. 2)

where n<sub>i</sub> is the number of droplets with diameter d<sub>i</sub>. On the other hand, span values aregiven by:

141 
$$Span = \frac{D(v,0.9) - D(v,0.1)}{D(v,0.5)}$$
 (Eq. 3)

where D(v, 0.9), D(v, 0.5) and D(v, 0.1) are the highest droplet size contained in 90%,
50% and 10% of volume of dispersed phase, respectively.

The physical stability of thyme essential oil emulsions is evaluated for 15 days at 30°C by means of a Turbiscan Lab Expert device (Formulaction, France) using the multiple light scattering technique. Emulsion stability is studied by analysing the variation of the backscattering (BS) profiles as a function of length of tube containing the sample, and time. This technique makes it possible to determine the major mechanisms of destabilization in each sample as well as the kinetics of the destabilization process.

# 151 2.6. Statistical Analysis

A one-way analysis of variance (ANOVA) was used to determine the occurrence of
significant differences among the obtained results. For this purpose, OriginPro 8 software
is used.

- 155 **3.- Results and Discussion.**
- 156 *3.1. Rheological properties*
- 157 3.1.1. Small amplitude oscillatory shear tests

Figure 1 shows stress sweeps at 1Hz as a function of welan gum concentration. Thanks 158 159 to this test, the linear viscoelastic range (LVR) can be measured, which indicates stress 160 region within which the response of the material does not depend on the applied stress. G' (storage modulus) and G'' (loss modulus) remain practically constant until a critical 161 stress ( $\tau_c$ ) is reached. From this point, generally, both moduli sharply decrease. However, 162 in these emulsions loss modulus values increase before the decrease. This behaviour is 163 164 observed in other systems and it can be explained by considering that a reorganization of the structure occurs before the nonlinear region is reached [13]. The critical stress value 165 166 is important because from this point the deformation in the structure is irreversible with increasing stress [12]. This parameter is often known as yield stress although it should be 167 168 noted that its value depends on the evaluation technique.

As can be observed in Figure 1, the linear viscoelastic range, and thus the critical stress 169 170 values, are clearly dependent on gum concentration. The critical stress values for emulsions are 0.06, 0.14, 0.36 and 0.59 Pa at 0.05 wt%, 0.1 wt%, 0.15 wt% and 0.2 wt% 171 172 of welan, respectively. This result indicates that increasing gum concentration in the 173 emulsions increases the resistance to shear, which implies a higher stability of the 174 emulsion under the stress amplitude. In addition, the storage modulus and the loss modulus values at the LVR slightly increase with increasing welan concentration, which 175 176 means an increase in the structural strength of the emulsions. Emulsions without gum do not present a linear viscoelastic response in the range of shear stress amplitude studied. 177

178

### Figure 1

In order to obtain more information concerning the linear viscoelastic properties, figure
2 illustrates the changes in G' and G"as a function of the frequency and the concentration
of welan gum for thyme oil/W emulsions aged for 24h. The results of these experiments

provide insights into the emulsion structure because these tests are non-destructive and 182 183 do not interfere with it. According to Steffe (1996) [14,15] and other authors, in weak gels, storage and loss moduli exhibit a slight dependence on frequency, and G' values 184 exceed G" values in the whole frequency range studied. Emulsions formulated with 185 thyme essential oil containing different concentrations of welan gum present clear 186 viscoelastic properties with a predominance of the elastic over the viscous component at 187 188 all frequencies and with both moduli practically independent of frequency. Therefore, 189 these emulsions behave as weak gel-like materials.

190

### Figure 2

191 The dependence of the storage modulus on the frequency can be quantitatively described192 by a power law type equation:

193 
$$G'(\omega) = K' \cdot \omega^{n'} \quad Eq. (4)$$

where K´ is the intercept and n´ is the slope in the double logarithmic plot of G´ againstfrequency.

196 The curves of G'as a function of angular frequency fit fairly well to the power law  $(R^2>0.99)$ . The fitting parameters are plotted in figure 3. The values for the slopes of G<sup> $\prime$ </sup> 197 198 (n') are similar for all welan gum concentrations, except for 0.1wt% which exhibits a 199 slight maximum value. This result indicates that no change in the structure occurs but 200 only a change of consistency of the system connected with the addition of welan gum 201 (thickening effect). The value of this slope also makes it possible to classify the behaviour of system. It is known that n' > 0 denotes weak gels whereas n' = 0 corresponds to strong 202 203 gels [16]. Our emulsions present n' values between 0.1 and 0.08 so it can be concluded 204 that these emulsions exhibit a weak gel-like behaviour. It is worth noting that a plateau 205 zone is obtained for the emulsion containing 0.05 wt% welan gum. The plateau zone is characterised by a trend of G'' to reach constant values at low frequencies. In this case a minimum value of G'' was achieved at 0.3 Hz.

208

### Figure 3

An increase in gum concentration causes a significant increase in G'and G". This rise can be related to the formation of a stronger and more elastic structure in the continuous phase [17]. The natural structure of welan gum is a perfect double helix [18]. As the gum concentration in the continuous phase of emulsions increases, the interaction between adjacent double helixes promotes the formation of a three-dimensional network that increases by increasing the gum concentration [19].

The dependence of the storage modulus, which is related to the solid-like response, on the welan concentration present in the emulsion is investigated. With this aim, the doublelogarithmic plot of G' at 1 rad/s against welan gum concentration is shown in Figure 4. The experimental data are well fitted ( $R^2 = 0.998$ ) to the following equation:

219 
$$G'_{1rad/s} = a \cdot C^b$$
 (Eq. 5)

As can be observed G' increases linearly with the concentration, the slope being 2.2. This value is close to that commonly found for normal polysaccharide gels at concentrations above the minimum critical gelling concentration (b = 2) [20]. The result obtained reveal that the rheology of these emulsions is dominated by the continuous phase.

224

## Figure 4

# 225 3.1.2. <u>Steady state flow test</u>

The emulsion formulated with no gum shows Newtonian behaviour and the flow curve fits fairly well to the Newtonian law. The viscosity value of 24 h aged Newtonian 228 emulsion is  $7.4\pm0.3$  mPa.s. When the different concentrations of gum are added, not only 229 is the rheological behaviour changed, but also an increase in viscosity occurs (Figure 5). 230 It is noteworthy that an increase in viscosity inhibits some destabilization processes such as creaming and/or phase separation by slowing down the droplet motion. Figure 5 shows 231 the influence of welan gum on the flow properties of thyme oil/W emulsions after an 232 aging time of 24 h. All emulsions containing gum show a pseudoplastic behaviour, with 233 234 viscosity versus shear rate exhibiting a trend to a viscosity plateau region at low shear 235 rates and, subsequently, a shear-thinning behaviour. Furthermore, it can be observed that the apparent viscosity  $(\eta)$  increases as the welan gum concentration increases, this being 236 237 due to the well-known thickening effect of polysaccharides. However, the increase in 238 viscosity exhibited for these emulsions may be also promoted by droplet flocculation which would be induced by the presence of welan in the continuous phase (depletion 239 240 flocculation). The greater the welan concentration, the greater the depletion flocculation 241 and the higher the viscosity. The fact that these emulsions are flocculated is consistent with the flow behaviour observed. The flocs act as a solid at low shear rate. Once the 242 critical shear rate is exceeded, the applied forces are sufficient to disrupt the bonds 243 244 between droplets and the emulsion flows, showing a shear thinning behaviour.

245 The behaviour found fits the Cross model fairly well ( $R^2 > 0.99$ ):

246 
$$\eta = \frac{\eta_0}{1 + \left(\frac{\gamma}{\gamma_c}\right)^{1-n}} \quad Eq. (6)$$

Where  $\gamma_c$  is related to the critical shear rate for the onset of the shear-thinning response,  $\eta_0$  stands for the zero-shear viscosity and (1-n) is a parameter related to the slope of the power-law region; n being the so-called "flow index". For shear thinning materials, n values are between 0 and 1. A solid material would show n = 0, while a Newtonian liquid would show n = 1.

For emulsions aged for 24 h, an increase in the gum concentration leads to an increase in 252 253 the zero shear viscosity (Table 1). It is worth noting that a small content of welan gum 254 causes a significant increment in emulsion viscosity (7.4 mPa·s in emulsion without gum versus 556 Pa s in emulsion containing only 0.05 wt% welan gum) due to, as mentioned 255 256 above, the thickening effect of welan. The  $\eta_0$  evolution is gradual from 0.05 wt% to 0.15 257 wt% of welan gum added to the emulsion, but a sudden increase in this parameter from 258 0.15 wt% to 0.2 wt% gum concentration was observed. This rheological change may be due to an improved viscosity of the continuous phase and/or a more marked effect of 259 260 depletion flocculation. In Table 1, we can also observe that there is a trend to decreasing 261 critical shear rate with increasing the gum concentration. In other words, the higher the 262 welan concentration in the emulsion, the narrower the Newtonian region. Regarding the flow index, significant differences with concentration were not observed. The values are 263 264 close to 0, indicating that emulsions containing welan gum exhibit a strong pseudoplastic 265 character.

266

## Figure 5

267

# Table 1

The flow curve results obtained are very interesting because they make it possible to control the viscosity of the thyme essential oil/W emulsions by adjusting the concentration of welan gum.

271 *3.2. Droplet size distribution* 

Figure 6 shows the droplet size distributions for all emulsions studied after an ageing time
of 24 h prepared with Silverson L5M at 2000rpm and one pass through the Microfluidizer
M110P at 2500psi. For these emulsification conditions, all emulsions formed present a
bimodal distribution as a consequence of the recoalescence phenomenon induced by an

excess of mechanical energy-input [21]. This result is usual in emulsions obtained with Microfluidizers [22]. Droplet size distribution shifts towards higher values with the addition of gum, and this effect is more marked from 0.15 wt% to 0.2 wt% welan gum concentration. Additionally, the second peak in droplet size distribution increases with increasing welan gum concentration.

281

## Figure 6

282 Except for the emulsion containing 0.2 wt% welan, all emulsions show submicron mean diameters. Figure 7 illustrates D3,2, D4,3 and span parameters as a function of gum 283 284 concentration. The incorporation of welan gum to thyme essential oil in water emulsions 285 causes an increase in both diameters (D3,2 and D4,3) and polydispersity. Subsequently, these parameters slightly increase with concentration until 0.2 wt% welan is reached. At 286 287 this gum concentration a significant increase in Sauter diameter, volume mean diameter and polydispersity occur. These results are consistent with those obtained from the flow 288 curves, where zero-shear viscosity also gradually increases up to 0.2 wt% welan, 289 concentration, at which point an important rise occurs. Again, this may be explained by 290 291 considering the depletion flocculation effect. This aggregation of droplets provokes an 292 increase in mean droplet size, which is more important at higher concentrations of welan 293 in the continuous phase.

294

### Figure 7

Microphotographs taken after one day for emulsions with different gum concentrations (Figure 8) also are in concordance with the increase in mean diameters and polydispersity as a function of welan concentration found by laser diffraction.

298

### Figure 8

#### 299 *3.3. Multiple Light Scattering*

Figure 9 illustrates, by way of example, the results of the physical stability study performed at room temperature by the multiple light scattering technique for emulsions containing 0 wt% (Figure 9a), 0.1 wt% (Figure 9b) and 0.2 wt% (Figure 9c). In this figure a plot of BS versus measuring cell height as a function of time is shown. Additionally, an inset is included where backscattering is plotted against tube length in reference mode  $(\Delta BS\% = BS\% - BS_0\%)$  to better show the backscattering changes.

306 Creaming is observed for the emulsion without gum (Figure 9a), which is the migration 307 of dispersed phase droplets from the lower area to the upper part of the sample due to the 308 difference in densities between the aqueous and dispersed phases. This destabilization is 309 also related to the low viscosity exhibited by this emulsion. Furthermore, it should be noted that  $\Delta BS\%$  decreases at the top of the tube length, which may be interpreted as a 310 311 coalescence process of droplets into the creamed phase [23]. No increase in droplet size implying flocculation, coalescence or Ostwald ripening is found in this emulsion, as can 312 be deduced from the lack of variation in the backscattering profiles from the middle of 313 314 the tube.

315 The addition of welan gum to the emulsion, in spite of increasing the viscosity of the 316 emulsion, fails to inhibit the creaming, although the clarification height decreases. It also causes a slight increase in droplet size with ageing time due to a destabilization 317 mechanism such as flocculation, coalescence or Ostwald ripening. Additionally we can 318 319 observe in Figure 9b a clarification at the top of the measuring cell. This result can be attributed to the occurrence of some coalescence which led to an oiling-off process (phase 320 321 separation). The increase in droplet sizes with ageing time is very slight up to 0.2 wt% welan concentration. At this concentration, this phenomenon is quite significant, as well 322

as a phase separation in the upper part of the sample. In order to quantify this phenomenon, the kinetics of the destabilization process in the middle zone of the measuring cell (between 20 and 25 mm of sample height) was studied. The  $\Delta$ BS (%) of each concentration has been plotted as a function of aging time in figure 10 and the results are fitted to an exponential equation (R2 > 0.99), typically used for a first- order kinetic model:

329 
$$\Delta BS = \Delta BS_E + (\Delta BS_0 - \Delta BS_E) \cdot exp(-kt) \quad Eq. (7)$$

where  $\Delta BS$  stands for the variation in the BS as a function of aging time,  $\Delta BS_E$  is the 330 corresponding decrease in BS when equilibrium is reached, BS<sub>0</sub> is the initial value of 331 backscattering, and k is the first-order kinetic coefficient. This kinetic equation has 332 333 proved to be useful to monitor the physical stability of oil-in-water emulsions [24]. Table 334 2 lists the values of the parameters of equation 7 as a function of welan gum concentration. 335 The first-order kinetic coefficient (k), the most relevant parameter, exhibits a tendency to 336 increase with the rise in the relative concentration of the welan gum, indicating a higher rate of increase in droplet size. Nevertheless, the low values of this parameter should be 337 noted for emulsions with smaller gum concentrations. In contrast, the emulsion with a 338 339 greater gum content (0.2wt%) exhibits higher values of k, indicating a significant increase in droplet size with aging time. These results are in concordance with those previously 340 341 obtained from flow curves and droplet size distribution. The incorporation of gum into the aqueous phase of emulsions causes an increase in both droplet size and viscosity, the 342 thickening effect and depletion flocculation being the responsible factors. This 343 aggregation of droplets continues with time, leading to coalescence and, finally, 344 345 provoking phase separation. The greater the welan content in the emulsion, the greater the phase separation. 346

347	Figure 9
348	Figure 10
349	Table 2

350

## 351 **4.-Conclusions.**

352 Thyme essential oil-in-water emulsions of submicron range were obtained with microfluidizer M100P at 2500psi-one pass using a bio-based surfactant called Appyclean 353 354 6548. In order to improve the rheological properties of emulsions, welan gum 355 polysaccharide was included in the emulsion formulation at different concentrations. 356 Emulsion without gum does not exhibit linear viscoelastic region. All the emulsions with gum show a weak-gel like behaviour with stronger interactions as the welan concentration 357 358 in the emulsion increases. Flow curves of emulsions containing gum exhibit a shear 359 thinning behaviour and they are fitted to the Cross-model equation. The viscosity of these 360 emulsions also increases with concentration of welan. Conversely, the emulsion without gum shows Newtonian behaviour. Multiple light scattering indicates that creaming is the 361 362 main destabilization mechanism for emulsion without gum. Creaming is decreased by the 363 better rheological properties of emulsions with polysaccharide. However, an increase in 364 droplet size, probably due to flocculation, occurs, this being significant at 0.2wt% welan gum. This emulsion shows the highest kinetics of destabilization. From the results 365 366 obtained, it can concluded that welan gum is an excellent rheological modifier of thyme essential oil/W emulsions, making it possible to control the viscosity of the emulsion by 367 368 adjusting its concentration. However, welan gum is not effective in increasing the physical stability of these emulsions. The main destabilization process is flocculation, 369 370 which finally provokes phase separation.

## 371 Acknowledgements

- 372 The financial support received (Project CTQ2015-70700-P) from the Spanish
- 373 Ministerio de Economía y Competitividad and from the European Commission
- 374 (FEDER Programme) is kindly acknowledged.

## 375 **References**

- K.J. Vander, L.L. Schramm, The effect of shear and oil/water ratio on the
  required hydrophile-lipophile balance for emulsification, J. Surfactants Deterg. 5
  (2002) 19–24. doi:10.1007/s11743-002-0200-6.
- 379 [2] M.J. Martin, L.A. Trujillo, M.C. Garcia, M.C. Alfaro, J. Muñoz, Effect of
- 380 emulsifier HLB and stabilizer addition on the physical stability of thyme essential
- oil emulsions, J. Dispers. Sci. Technol. 0 (2018) 1–8.
- doi:10.1080/01932691.2018.1459677.
- 383 [3] V. Fréville, E. Van Hecke, C. Ernenwein, A. Salsac, I. Pezron, Effect of
- 384 Surfactants on the Deformation and Detachment of Oil Droplets in a Model
- 385 Laminar Flow Cell, Oil & Gas Science and Technology–Revue d'IFP Energies

386 nouvelles 69(3) (2013) 435-444. doi:10.2516/ogst/2013110.

- 387 [4] P. Kurdi, C. Hansawasdi, Assessment of the prebiotic potential of
- 388 oligosaccharide mixtures from rice bran and cassava pulp, LWT Food Sci.

389 Technol. 63 (2015) 1288–1293. doi:10.1016/J.LWT.2015.04.031.

- 390 [5] J. Weiss, S. Gaysinsky, M. Davidson, J. McClements, Nanostructured
- 391 Encapsulation Systems: Food Antimicrobials, Glob. Issues Food Sci. Technol.
- 392 (2009) 425–479. doi:10.1016/B978-0-12-374124-0.00024-7.
- 393 [6] J. Nguefack, O. Tamgue, J.B.L. Dongmo, C.D. Dakole, V. Leth, H.F. Vismer,

394		P.H. Amvam Zollo, A.E. Nkengfack, Synergistic action between fractions of
395		essential oils from Cymbopogon citratus, Ocimum gratissimum and Thymus
396		vulgaris against Penicillium expansum, Food Control. 23 (2012) 377–383.
397		doi:10.1016/j.foodcont.2011.08.002.
398	[7]	C. Turek, F.C. Stintzing, Stability of Essential Oils: A Review, Compr. Rev.
399		Food Sci. Food Saf. 12 (2013) 40–53. doi:10.1111/1541-4337.12006.
400	[8]	S. Burt, Essential oils: their antibacterial properties and potential applications in
401		foods-a review, Int. J. Food Microbiol. 94 (2004) 223-253.
402		doi:10.1016/J.IJFOODMICRO.2004.03.022.
403	[9]	Y. Zhang, Z. Zhang, X. Li, W. Li, X. Shen, H. Wang, Effect of welan gum on the
404		hydration and hardening of Portland cement, J. Therm. Anal. Calorim. 131
405		(2018) 1277–1286. doi:10.1007/s10973-017-6589-5.
406	[10]	L. Xu, G. Xu, T. Liu, Y. Chen, H. Gong, The comparison of rheological
407		properties of aqueous welan gum and xanthan gum solutions, Carbohydr. Polym.
408		92 (2013) 516–522. doi:10.1016/J.CARBPOL.2012.09.082.
409	[11]	V. Kaur, M.B. Bera, P.S. Panesar, H. Kumar, J.F. Kennedy, Welan gum:
410		Microbial production, characterization, and applications, Int. J. Biol. Macromol.
411		65 (2014) 454–461. doi:10.1016/J.IJBIOMAC.2014.01.061.
412	[12]	L.A. Trujillo-Cayado, M.C. Alfaro, J. Muñoz, A. Raymundo, I. Sousa,
413		Development and rheological properties of ecological emulsions formulated with
414		a biosolvent and two microbial polysaccharides, Colloids Surfaces B
415		Biointerfaces. 141 (2016) 53–58. doi:10.1016/j.colsurfb.2015.11.046.
416	[13]	F. Rincón, J. Muñoz, P. Ramírez, H. Galán, M.C. Alfaro, Physicochemical and

417		rheological characterization of Prosopis juliflora seed gum aqueous dispersions,
418		Food Hydrocoll. 35 (2014) 348–357. doi:10.1016/J.FOODHYD.2013.06.013.
419	[14]	J.F. Steffe, Rheological methods in food process engineering, second ed.,
420		Freeman press, USA, 1996. doi:10.1016/0260-8774(94)90090-6.
421	[15]	A. Martínez-Ruvalcaba, E. Chornet, D. Rodrigue, Viscoelastic properties of
422		dispersed chitosan/xanthan hydrogels, Carbohydr. Polym. 67 (2007) 586-595.
423		doi:10.1016/J.CARBPOL.2006.06.033.
424	[16]	K.W. Song, H.Y. Kuk, G.S. Chang, Rheology of concentrated xanthan gum
425		solutions: Oscillatory shear flow behavior, Korea Aust. Rheol. J. 18 (2006) 67-
426		81. doi:10.1007/BF02908257.
427	[17]	A.S. Tomé, C. Pires, I. Batista, I. Sousa, A. Raymundo, Protein gels and
428		emulsions from mixtures of Cape hake and pea proteins, J. Sci. Food Agric. 95
429		(2015) 289–298. doi:10.1002/jsfa.6717.
430	[18]	E.R. Morris, M.G.E. Gothard, M.W.N. Hember, C.E. Manning, G. Robinson,
431		Conformational and rheological transitions of welan, rhamsan and acylated
432		gellan, Carbohydr. Polym. 30 (1996) 165-175. doi:10.1016/S0144-
433		8617(96)00059-8.
434	[19]	L. Xu, Z. Qiu, H. Gong, C. Liu, Y. Li, M. Dong, Effect of diutan microbial
435		polysaccharide on the stability and rheological properties of O/W nanoemulsions
436		formed with a blend of Span20-Tween20, J. Dispers. Sci. Technol. 39 (2018)
437		1644–1654. doi:10.1080/01932691.2018.1461636.
438	[20]	A.H. Clark, S.B. Ross-Murphy, Structural and mechanical properties of

439 biopolymer gels, in: Biopolymers, Springer Berlin Heidelberg, Berlin,

- 440 Heidelberg, 1987: pp. 57–192.
- 441 [21] S.M. Jafari, Y. He, B. Bhandari, Optimization of nano-emulsions production by
  442 microfluidization, Eur. Food Res. Technol. 225 (2007) 733–741.
- 443 doi:10.1007/s00217-006-0476-9.
- 444 [22] L.A. Trujillo-Cayado, M.C. Alfaro, J. Santos, N. Calero, J. Muñoz, Influence of
- 445 primary homogenization step on microfluidized emulsions formulated with
- 446 thyme oil and Appyclean 6548, J. Ind. Eng. Chem. 66 (2018) 203–208.
- 447 doi:10.1016/J.JIEC.2018.05.031.
- 448 [23] G.G. Palazolo, D.A. Sorgentini, J.R. Wagner, Coalescence and flocculation in

o/w emulsions of native and denatured whey soy proteins in comparison with soy

- 450 protein isolates, Food Hydrocoll. 19 (2005) 595–604.
- 451 doi:10.1016/J.FOODHYD.2004.10.022.
- 452 [24] M.C. García, M.C. Alfaro, N. Calero, J. Muñoz, Influence of polysaccharides on
- 453 the rheology and stabilization of  $\alpha$ -pinene emulsions, Carbohydr. Polym. 105
- 454 (2014) 177–183. doi:10.1016/j.carbpol.2014.01.055.

# 455 Tables

449

Table 1. Fitting parameters to the Cross model for emulsions studied. Standard deviation of the mean (2 replicates) for  $\eta_{\infty} < 2\%$ ,  $\eta_0 < 10\%$ ,  $\dot{\gamma} < 1\%$  and n < 5%.

Welan gum concentration (wt%)	n	$\eta_{\infty}$ (Pa.s)	$\eta_0$ (Pa.s)	γ̈́ (s <sup>-1</sup> )
0.05	0.14	0.015	556	1.5,10-4
0.1	0.18	0.017	2103	1.1,10 <sup>-4</sup>
0.15	0.13	0.03	5736	4.8,10-5
0.2	0.16	0.033	17514	5.6,10 <sup>-5</sup>

Welan gum concentration (wt%)	$\Delta BS_{E}$ (%)	$\frac{\mathbf{BS}_0 - \Delta \mathbf{BS}_{\mathrm{E}}}{(\%)}$	K (s <sup>-1</sup> )	R <sup>2</sup>
0	-1.05	1.17	4.38	0.95
0.05	-1.36	1.35	1.69	0.98
0.1	-2.65	2.54	2.74	0.99
0.15	-2.10	2.04	3.77	0.97
0.2	-38.38	40.20	4.03	0.97

Table 2. Fitting parameters of the first-order kinetic equation for the BS in the 20–25 mm
zone of the measuring cell versus aging time as a function of welan gum concentration.

462

#### 463 **Table captions**

464 Table 1. Fitting parameters to the Cross model for emulsions studied. Standard deviation 465 of the mean (2 replicates) for  $\eta_{\infty} < 2\%$ ,  $\eta_0 < 10\%$ ,  $\dot{\gamma} < 1\%$  and n < 5%.

Table 2. Fitting parameters of the first-order kinetic equation for the BS in the 20–25 mm
zone of the measuring cell versus aging time as a function of welan gum concentration.

### 468 **Figure captions**

- 469 Figure 1. Oscillatory shear stress sweeps as a function of welan concentration. 470 Temperature =  $25 \,^{\circ}C$
- 471 Figure 2. Mechanical spectra of emulsions as a function of welan gum concentration.
  472 Standard deviation for the mean is also plotted. Temperature = 25 °C
- 473 Figure 3. Fitting parameters to the power law equation for all the emulsions studied. K<sup>-</sup>
- 474 is the intercept and n´ is the slope in the double logarithmic plot of G´ against frequency475 as a function of welan gum concentration.
- Figure 4. Storage modulus versus welan gum concentration. Continuous lines illustrate the data fitting to the power law. Standard deviation for the mean is also plotted. Temperature =  $25 \,^{\circ}$ C.

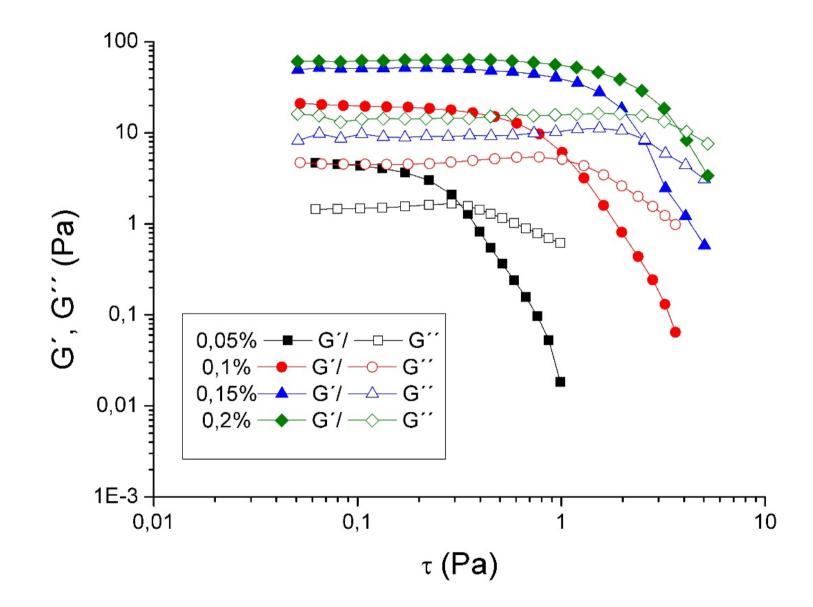
458

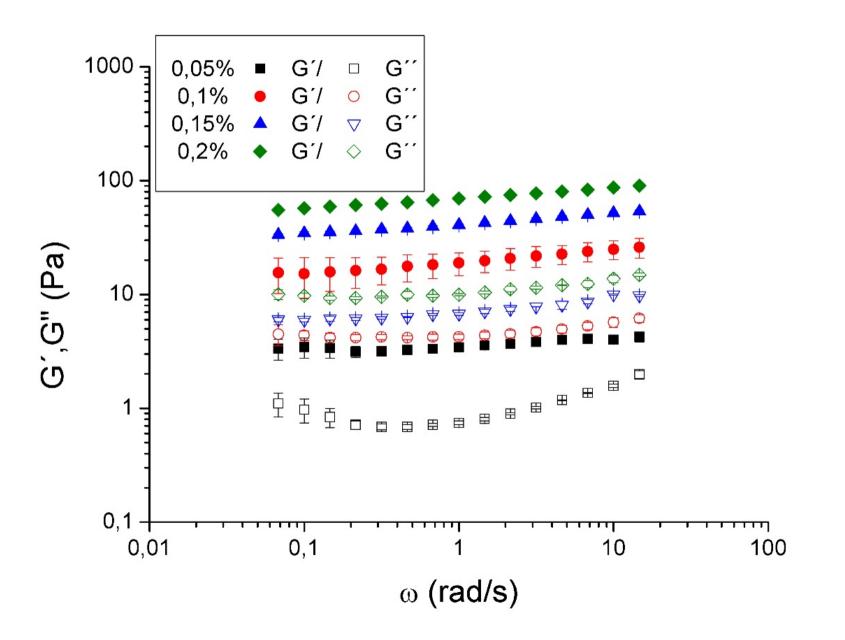
459

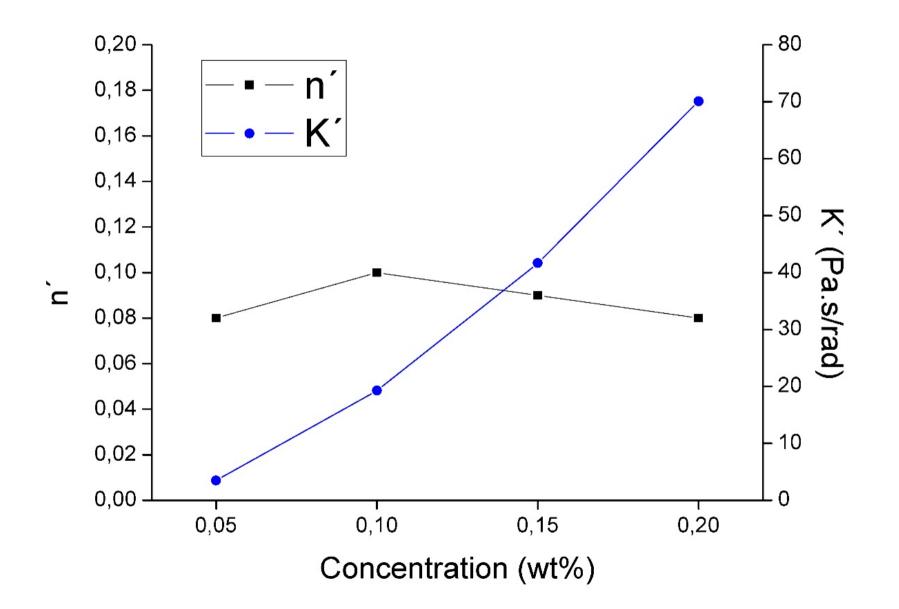
- 479 Figure 5. Flow curves of emulsions aged for 24 as a function of welan gum concentration.
- 480 Continuous lines illustrate the data fitting to the Cross equation. Temperature = 25 °C. 481 Standard deviation of the mean (two replicates) for  $\eta < 8\%$ .
- 482 Figure 6. Droplet size distributions for emulsions aged for 24 h as a function of welan483 gum concentration.
- 484 Figure 7. Sauter mean diameters, volumetric mean diameters and span for all emulsions485 aged for 24 h as a function of welan gum concentration.
- Figure 8. Photomicrographs for all emulsions prepared as a function of welan gum
  concentration a) without gum, b) 0.05wt%, c) 0.1wt%, d) 0.15wt% and e) 0.2wt% at 24
  h of aging time.
- 489 Figure 9. Backscattering versus measuring cell height as a function of time and reference
- 490 mode (insets) for emulsions made a)without gum, b)0.1wt% welan gum and c) 0.2wt%
  491 welan gum, at 25°C.
- 492 Figure 10. Destabilization kinetics in the 20–25 mm zone monitored over 15 days for all
  493 studied emulsions as a function of welan gum concentration.

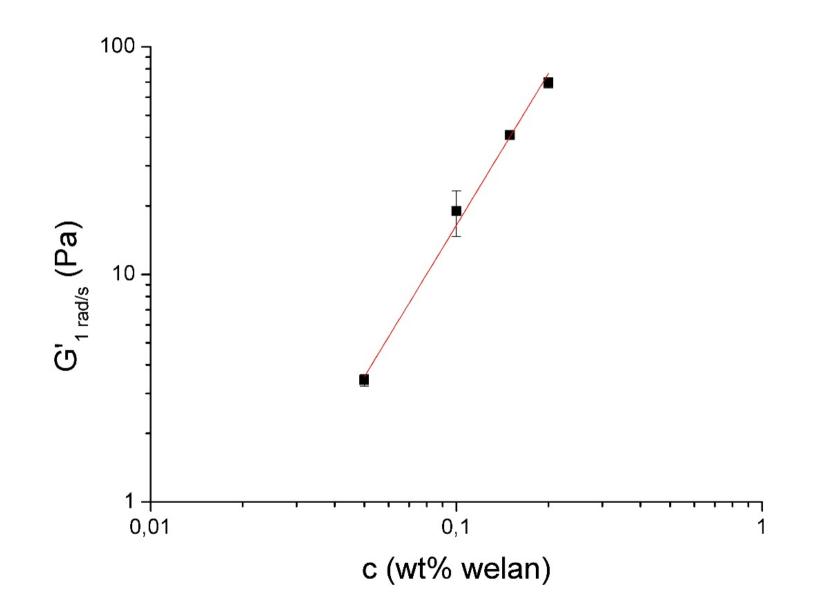
494

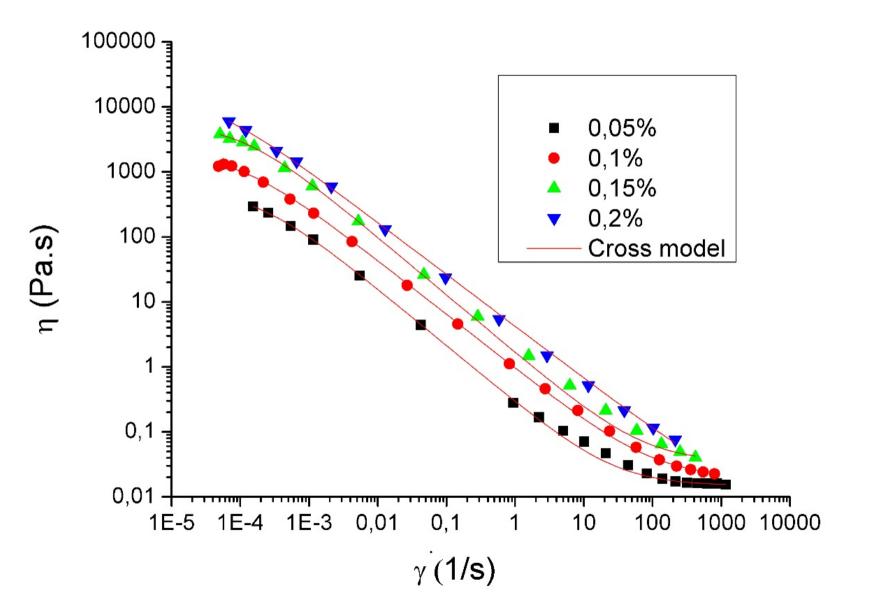
495

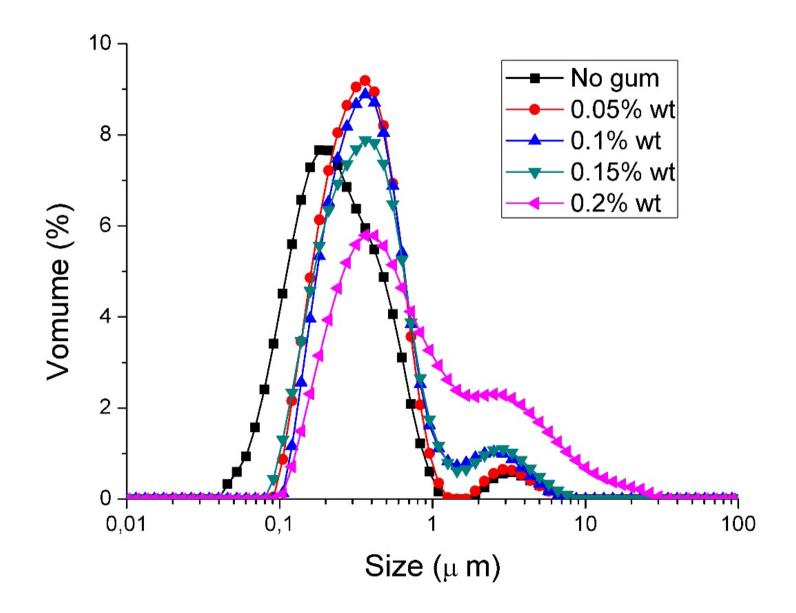


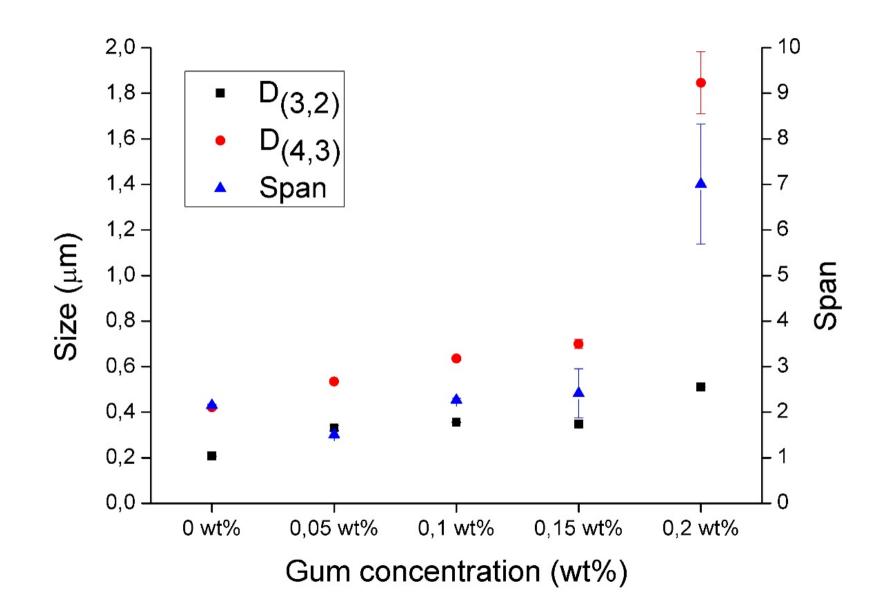


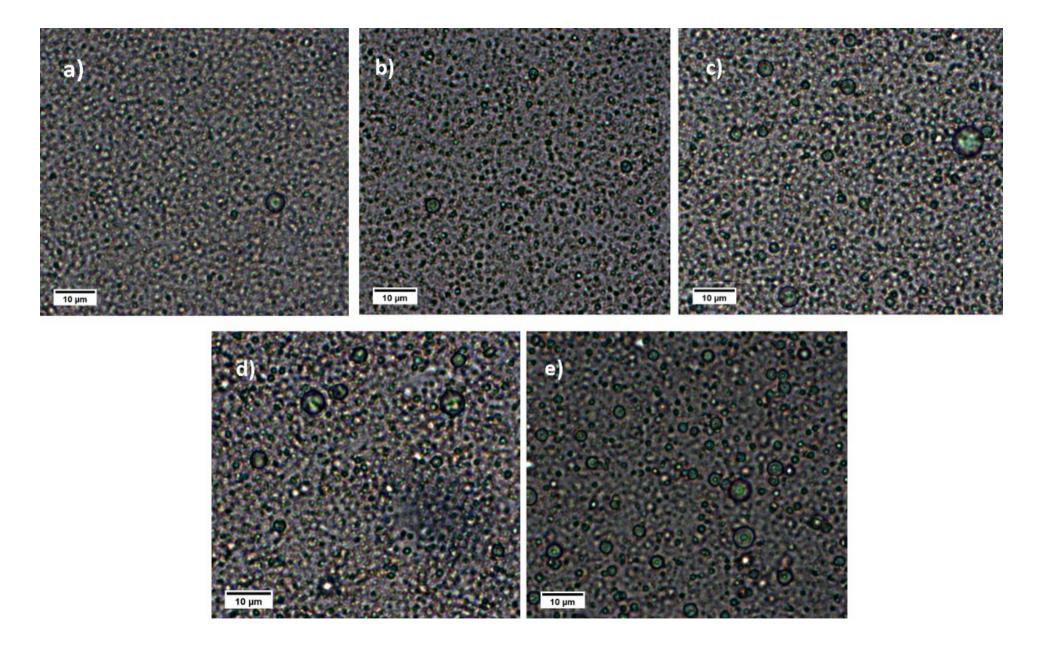


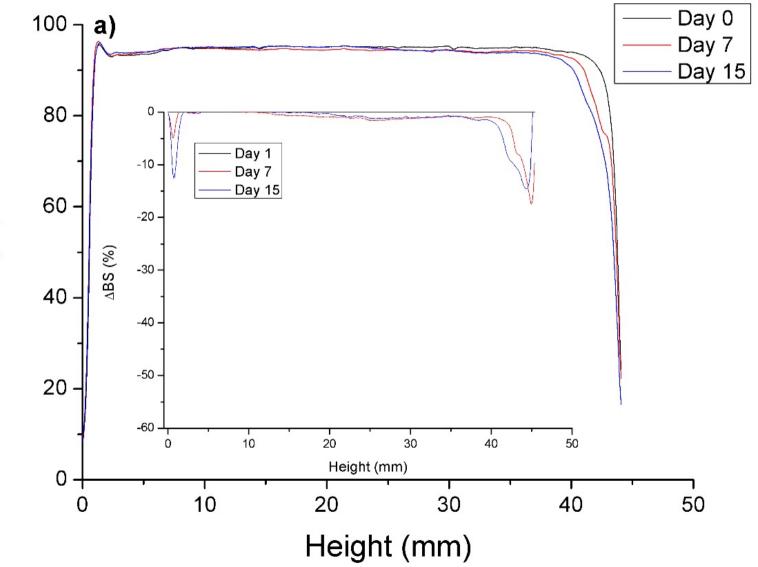












BS(%)

