

Phenolic compounds from virgin olive oil obtained by natural deep eutectic solvent (NADES): effect of the extraction and recovery conditions

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1 **Phenolic compounds from virgin olive oil obtained by natural deep eutectic solvent**
2 **(NADES): effect of the extraction and recovery conditions**

3

4 **Abstract**

5 Environmentally friendly natural deep eutectic solvents (NADES) have been shown to
6 efficiently extract a wide range of phenolic compounds from virgin olive oil (VOO). The
7 objective of this work was to optimize the yield of olive oil phenols extracted by NADES
8 based on choline chloride/xylitol (Xyl/ChCl). Different extraction and recovery
9 conditions were investigated, including the effect of different extraction operating
10 parameters (temperature, time, VOO:NADES ratio) and subsequent recovery conditions
11 (XAD resin height, wash-water and eluent volume and pH). The highest concentration of
12 phenols (555.36 mg/kg VOO) was obtained from extraction at 40° C for 1 h, with a 1:1
13 ratio, using an adsorption resin XAD-16 with bed height of 10 cm, 250 mL acidified
14 wash-water and 300 mL EtOH 100% as eluent. No statistically significant loss of the sum
15 of phenolic compounds was observed when compared with the concentration values
16 obtained by direct analysis in HPLC without the elimination of NADES. Additionally, a
17 sequential desorption with different concentration of ethanol was used to determine the
18 effect of the solvent concentration on polyphenol yield. Polar compounds, such as
19 hydroxytyrosol and tyrosol, were recovered at 81.7 % and 83.6 %, respectively; however,
20 100% ethanol was required for the complete elution of oleacein (3,4-DHPEA-EDA) and
21 oleocanthal (*p*-HPEA-EDA). In this paper we present an effective process for the extraction of
22 polyphenols from VOO by NADES for direct analysis in HPLC and for the recovery and
23 concentration of polyphenols by removing the solvent (NADES) with no losses of yield and
24 solvent recycling.

25 **Keywords**

26 **Phenolic compounds, Natural Deep Eutectic Solvent, Virgin Olive Oil, Extraction,**
27 **Recovery.**

28

29 **Introduction**

30 Natural deep eutectic solvents (NADES) are currently an alternative to conventional
31 solvents for the extraction of phytochemicals, such as phenolic compounds, from diverse
32 sources, among them olive fruits and derived products including olive oil (Ferrone et al.
33 2018; Garcia et al. 2016). In the present day, consumers demand natural bioactive
34 products for multiple purposes, which have been obtained using sustainable production
35 techniques, challenging many conventional procedures. Many organic solvents, e.g.,
36 alcohols, chloroform, and ethyl acetate, are still extensively employed for extraction of
37 biologically active compounds (Gavahian et al. 2019; Mark et al. 2019; Francisco et al.
38 2019), although they contribute to environmental pollution and leave undesirable solvent
39 deposits in the extracts. This is the reason why significant progress has recently been
40 made in the development of new extraction methods for substances of interest, such as
41 phenolic compounds, that avoid or minimize the use of organic solvents, and that allow
42 obtaining extracts or purified compounds, useful both in research and in the food,
43 pharmaceutical or cosmetic industries.

44 An alternative to these solvents are the so-called NADES (Dai et al. 2013a), a group of
45 eco-friendly solvents (Jiang et al. 2019; Athanasiadis et al. 2018), with properties such
46 as low volatility at room temperature, non-flammability, a wide range of polarity, and
47 high biodegradability. Dai et al. (2014) included the term NADES to define liquids

48 obtained from natural products as primary metabolites, including organic acids, amino
49 acids, sugars, alcohol or amines with a wide variety of applications (Dai et al. 2013b).
50 NADES are considered to form an ionic bond to give a liquid crystal at room temperature
51 whose melting temperature is much lower than that of the starting components. Such
52 interactions are formed by the combination of compounds of high melting point, generally
53 solid to form a liquid due to the delocalization of the charge, caused by hydrogen bonding,
54 generating a eutectic point whose melting temperature is much lower than the starting
55 compounds. Since NADES are constituted by natural and innocuous substances, they are
56 very interesting for the extraction of bioactive compounds from different matrices (Dai et
57 al. 2013c).

58 Phenolic compounds are a group of structurally diverse secondary metabolites in plants
59 that are essential for plant growth, development, stress adaptation, and defense and exhibit
60 numerous beneficial properties for health (Villard et al. 2019; Gutierrez et al. 2019). They
61 have attracted a large amount of interest in recent years due to their antioxidant capacity
62 (Franco et al. 2014; Fuentes et al. 2018), which has been associated with beneficial
63 effects for health, such as a reduced risk of coronary heart disease, prevention of several
64 types of cancers (Reboredo-Rodríguez et al. 2018), modification of immune and
65 inflammatory responses, antihypertension, antimicrobial and cholesterol-lowering
66 properties (Hounsome et al. 2008).

67 Virgin olive oil (VOO) contains at least 30 phenolic compounds, whose main classes are
68 secoiridoids aglycons such as the dialdehydic forms of elenolic acid linked to
69 hydroxytyrosol (3,4-DHPEA-EDA) or tyrosol (*p*-HPEA-EDA), oleuropein and ligstroside
70 aglycons (3,4-DHPEA-EA, *p*-HPEA-EA) respectively, phenolic alcohols such as
71 hydroxytyrosol (Hy) and tyrosol (Ty), the lignans acetoxypinoresinol and pinoresinol,
72 and flavonoids such as luteolin and apigenin. Most phenolic compounds present a broad

73 spectrum of antioxidant, free radical scavenger and anti-inflammatory effects and their
74 biological properties have been wide investigated (Serreli and Deiana 2018). Among
75 them, secoiridoid derivatives of oleuropein and ligstroside are considered bioactive
76 compounds because they can be hydrolyzed to Hy before reaching human plasma (Fitó et
77 al. 2007). In addition, *p*-HPEA-EDA has demonstrated anti-inflammatory activity with
78 the ability to inhibit COX-1 and COX-2 enzymes similar to ibuprofen (Beauchamp et al.
79 2005). Furthermore, this phenolic compound is able to inhibit the phosphorylation of c-
80 Met kinase in vitro, a proto-oncogene receptor with a significant oncogenic role in many
81 tumors, (Akl et al. 2014) and suppress the growth of luminal breast cancer cells, in part,
82 by reducing total levels of ER α in cell culture and animal studies (Ayoub et al. 2017).
83 The antibacterial effect of 3,4-DHPEA-EDA against a broad spectrum of bacteria is also
84 well described, together with its antioxidant and antiproliferative properties (Castro et al.
85 2007). Lignans such as acetoxypinoresinol and pinoresinol possess antioxidant activity
86 and they have been associated with antitumor effects. Pinoresinol exerts anti-inflammatory
87 activity and antifungal activity against several human pathogen fungi, neuroprotective
88 and hypoglycaemis actions (López-Biedma et al. 2016). Flavonoids like apigenin and
89 luteolin showed effect in suppressing colorectal cancer cell by slowing their growth by
90 cell cycle arrest. (Borzi et al. 2019). Phenolic compounds in olive oil have been
91 traditionally extracted by means of organic solvents such as methanol, ethanol, their
92 aqueous mixtures or others solvents such as *N,N*-dimethylformamide, with liquid-liquid
93 or solid-phase extraction (Brenes et al. 2000). In the organic solvent extraction,
94 parameters such as the ratio VOO:solvent, temperature or the extraction time are slightly
95 variable. Phenolic compounds in oil such as secoiridoids derivatives can be hydrolyzed
96 with high temperature when extracted and concentrated with organic solvents or their
97 aqueous mixtures, for that reason, temperatures below 35 °C are used to obtain a phenolic

98 extract without hydrolyzing. The official method for extraction of phenolic compounds
99 from VOO by the International Olive Council Testing Method uses 80% (v/v) methanol
100 at room temperature. However, Garcia et al. (2016) demonstrated that extraction of
101 phenolic compounds from the VOO by eutectic solvents was more effective than
102 extraction by methanol 50% or 80% (v/v) at temperature of 40°C. The removal of organic
103 solvent for the concentration of polyphenols from the extracts is done by low temperature
104 evaporation. For the removal of eutectic solvents from phenolic extracts, resin adsorption
105 was used, it is not known how different parameters of this process affect the phenolic
106 content of the extracts.

107 However, different factors can affect the extraction and recovery of phenolic compounds
108 from VOO. The objective of this work was to determine the optimal conditions for the
109 extraction and recovery of phenolic compounds from VOO using an NADES-based
110 method.

111

112 **Materials and Methods**

113 **Samples, standards, and reagents**

114 VOO of the Hojiblanca variety was purchased from commercial suppliers and preserved
115 at -20° C until its use. The standard compounds tyrosol, luteolin, apigenin and pinoresinol
116 were purchased from Sigma-Aldrich (St. Louis, MO). Hydroxytyrosol was obtained by
117 the method described by Fernández-Bolaños et al. (2004). Oleacin, oleocanthal,
118 oleuropein aglycone, ligstroside aglycone and 1-acetoxypinoresinol were obtained from
119 VOO separated in an analytic C-18 column and eluted with MeOH:H₂O, as described by
120 García et al. (2001). HPLC grade methanol was purchased from Panreac-Applichem.
121 Milli-Q water was used acidified with 6N TFA.

122 Xylitol, and 1,2-choline chloride were obtained from Sigma Aldrich. Resin Amberlite
123 XAD-16 was purchased from Vivaqua, Spain.

124

125 **Preparation of Natural Deep Eutectic Solvent (NADES)**

126 Natural deep eutectic solvent (NADES) was prepared according to the evaporating
127 method described by Dai et al. (2013b). Briefly, a choline chloride, xylitol and water
128 mixture (ChCl:Xyl:Water) with a ratio (2:1:3) was heated with a rotary evaporator in a
129 round-bottomed flask until a homogeneous colorless liquid was formed.

130 **Extraction of phenolic compounds**

131 The control extraction procedure was performed by mixing 14 g VOO with 14 g of
132 NADES with agitation in a water bath at 40 °C for 1 h. The 1:1 VOO: NADES mixture
133 was centrifuged at 1200 g during 10 min and the NADES-phase was recovered. This
134 procedure was repeated and the extracts pooled. The extract was analyzed by direct
135 injection in HPLC without elimination of NADES. The NADES phase was washed four
136 times with hexane to eliminate residual oil and bubbled with nitrogen to eliminate residual
137 hexane.

138 In order to evaluate the effect of different conditions on the extraction of polyphenols, the
139 procedure described above was modified. To investigate the effect of extraction time,
140 extraction times of 0.5 h, 2 h and 6 h were used and compared to the control time of 1 h
141 at a temperature of 30 and 40 °C and with a 1:1 VOO: NADES ratio. The effect of
142 temperature on the extraction was analyzed at 30, 60 and 90 °C and compared to the
143 control temperature of 40 °C, with extraction time 1 h and 1:1 VOO: NADES ratio.
144 Finally, the effect of the VOO: NADES ratio was determined applying the ratios 1:3, 1:4,

145 1:7, and compared to the 1:1 control ratio with an extraction time of 1 h and temperature
146 of 40 °C.

147 **Recovery of phenolic compounds**

148 NADES extracts (20 mL) were passed through an amberlite XAD-16 adsorbent filled
149 column with 2.3 cm inside diameter to give a bed height of 10 cm. The adsorbent was
150 pre-treated with 50 mL of ethanol and washed with 50 mL of MQ water prior to loading
151 of the phenolic extracts. Extracts were washed with 250 mL of MQ water and the captured
152 phenols eluted from the resin with 300 mL of ethanol 100%. Eluted samples were dried
153 under vacuum at 30 °C, dissolved in 1 mL of MeOH and filtered through a 0.45 µm nylon
154 filter for analysis by HPLC-DAD. This procedure was considered the control recovery
155 protocol.

156 The control conditions that had been used in the recovery of phenols were modified to
157 determine their possible effect on the final concentration. For this, the effect of column
158 bed height on the adsorption of phenolic compounds from the NADES extract was
159 analyzed, using 10 cm, control height, and doubling it to 20 cm. In the processes of pre-
160 treatment of the column and elution of the phenols, all volumes were doubled with respect
161 to the control. Thus, 100 mL of ethanol followed by 100 mL of MQ water were used in
162 the pre-treatment of the adsorbent, then 20 mL of NADES extract was loaded, it was
163 washed with 500 mL of MQ water, and then eluted with 600 mL of 100% ethanol.

164 The possible effect of pH on the recovery of phenolic compounds from the extract was
165 studied. Thus, the washing water used during the pretreatment of the column and in the
166 phenol elution process, was adjusted to pH 4 with acetic acid. The possible effect of the
167 type of solvent, ethanol or methanol used in the column pre-treatment and phenol
168 recovery processes was also determined.

169 Finally, the effect of the aqueous solvent mixtures on the desorption of the polyphenols
170 was assayed using a column bed of 20 cm, with sequential elution performed with 100
171 mL of 50, 80 and 100% ethanol.

172 **HPLC-DAD analysis of phenolic compounds**

173 The chromatographic system consisted of a HP 1100 Series gradient HPLC (Agilent
174 Technologies, Santa Clara, California). A Mediterranea SEA 18 column (250 mm 4.6 mm
175 i.d. 5 μ m, Teknokroma, Barcelona, Spain) was used for the separation. Detection was
176 performed with a HP diode array detector (DAD): the wavelength used for the
177 quantification of luteolin and apigenin was 340 nm, and 280 nm for the rest of the
178 compounds. The mobile phases used to perform the separation consisted of methanol and
179 water. Elution was achieved using an elution gradient with an initial composition of 90%
180 water (with pH adjusted to 2.5 with 6 N trifluoroacetic acid) and 10% methanol. The
181 concentration of methanol was increased to 30% in 10 min and maintained for 10 min.
182 Then, the methanol percentage was raised to 40% in 10 min and maintained for 5 min.
183 Finally, the methanol percentage was increased to 60%, 70%, and 100% in 5-min periods.
184 The initial conditions were reached in 15 min. The flow rate used was 1 mL/min.
185 Quantification of phenolic compounds was performed using the reference compounds
186 obtained from commercial suppliers or preparative HPLC, as previously described
187 (Section 2.1). The concentration of polyphenols was expressed in mg/kg of VOO.

188 **Statistical analysis**

189 All studies were performed in duplicate and means and standard deviations were
190 calculated. One-way and two-way statistical analyses were completed by ANOVA test

191 using IBM.SPSS Statistics (Version 25). The significance of the results was compared
192 using $p < 0.05$.

193

194 **Results and discussion**

195 NADES are solvents that allow the efficient extraction of molecules, including
196 polyphenols, from different matrices such as olive oil. In this work, we performed the
197 extraction of polyphenols from VOO using a NADES formulation based on Xyl/ChCl
198 that was chosen for its high extractive efficiency compared to other NADES formulations
199 and conventional solvents (García et al. 2016). The most favorable conditions for
200 obtaining phenolic compounds and eliminating the solvent from the extracts by means of
201 adsorption resins were studied. This method permits the concentration of polyphenols for
202 later use.

203 The content of the phenolic compounds obtained from NADES extracts was determined
204 by quantitative analysis by HPLC-UV, the results are shown in Figure 1. A direct
205 injection analysis of the phenolic extract obtained without solvent removal was performed
206 by the control extraction procedure (Fig. 1a). The results were compared with those
207 obtained from the extract after solvent removal using the control recovery protocol (Fig.
208 1b). Direct injection of the extract is a useful analysis when no concentration of the
209 phenolic compounds in the extract is required. However, the use of concentrated solvent-
210 free phenolic extracts is useful in many analytical and industrial applications. Results
211 showed that chromatographic profiles of the two analytical determinations are similar.
212 The sum of all the polyphenols is also statistically similar. When analyzing the
213 compounds individually, the concentrations of secoiridoid aglucones were higher in the

214 concentrated extract while the alcohols hydroxytyrosol and tyrosol showed higher
215 amounts in the extract analyzed by direct injection, the differences were not statistically
216 significant except for hydroxytyrosol. These losses could have been produced by the
217 washing during the recovery stage of these highly water-soluble phenols. NADES have
218 low volatility, hence it was difficult to eliminate the solvent from the extracts obtained
219 and therefore the yield for downstream analytical applications is somewhat limited. In
220 order to concentrate the phenolic extracts obtained by NADES, methods such as the
221 adsorption of polyphenols to resins followed by elution with organic solvent can be used.
222 The effect of parameters – including time, temperature and ratio – on the capacity of
223 NADES to extract polyphenols from VOO were analyzed sequentially, and the optimal
224 extraction conditions for each parameter were defined. Figure 1b shows the
225 chromatogram of the phenolic compounds concentrated and obtained under optimal
226 extraction conditions.

227 **Effect of temperature**

228 The effect of different temperatures (30, 40, 60 and 90 °C) on the extraction efficiency of
229 the phenolic compounds from VOO obtained with Xylitol-Choline Chloride based
230 NADES (Xyl/ChCl-NADES) (g/g) in a 1:1 ratio during 1 h of extraction was evaluated.
231 The solvent exhibited a higher extractive capacity at 30 and 40 °C for the four most
232 abundant secoiridoid derivatives in VOO (Fig. 2a), with the most favorable temperature
233 being 40 °C for the extraction of 3,4-DHPEA-EDA (oleacein) and *p*-HPEA-EDA
234 (oleocanthal), followed by oleuropein aglycon (3,4-DHPEA-EA) and ligstroside aglycon
235 (*p*-HPEA-EA). The simple phenols hydroxytyrosol (Hy) and tyrosol (Ty) were extracted
236 in the highest concentrations at 30 and 40 °C for Hy and at 40 °C for Ty (Fig. 2b). The
237 extractability of these compounds decreased significantly ($p<0.05$) with the increase of

238 temperature from 40 to 60 and 90 °C. The increase in temperature may reduce the
239 viscosity of NADES and thus improve its extraction efficiency (Dai et al. 2013a;
240 Moghimi and Roosta 2019; Lapeña et al. 2019) and/or it could degrade secoiridoid
241 aglycons (Brenes et al. 2002; Lee et al. 2007). However, no increase was detected in the
242 simple molecules derived from hydrolysis, hence the increase in temperature decreased
243 the overall extraction capacity. For the rest of the phenolic compounds analyzed, the
244 lignans 1-acetoxypinoresinol and pinoresinol were stable at high temperatures (Brenes et
245 al. 2002), and neither significant differences in concentration of the flavonoids luteolin
246 and apigenin, which remained stable even at 60 and 90 ° C, nor improvements in the
247 extraction of phenols by NADES were observed. Therefore, temperatures of 30° and 40°
248 C were selected to perform the next experiment.

249 **Effect of extraction time**

250 The effect of extraction time at two different temperatures 30 and 40 °C was conducted
251 for the extraction of phenols during 0.5, 1, 2 and 6 h, with a 1:1 ratio of VOO: Xyl/ChCl-
252 NADES (g/g) (Table 1). The extract obtained with NADES at 40 °C for 1 h had the highest
253 concentration of the four secoiridoids, followed by the extraction at 0.5 h, which yielded
254 10%, 17% and 43% lower amounts of 3,4-DHPEA-EDA, *p*-HPEA-EDA and 3,4-
255 DHPEA-EA, respectively (Fig. 3). The amount of secoiridoids decreased significantly
256 with longer extraction times, with lowest yields at 6 h. This may reflect the degradation
257 of these compounds with longer extraction times, which occurred even at 30 °C. However,
258 a slight but significant increase of Hy and Ty was observed after 6 h of treatment at 40
259 °C, which could be related to the decrease in their secoiridoids derivatives by hydrolysis
260 and release of the phenolic alcohols, highest concentration of lignan 1-acetoxypinoresinol
261 was obtained for 6 h of extraction at 40 °C; this increase was also detected after 6 h at 30

262 °C which would correspond with the greater stability of the lignans. The rest of the
263 phenolic compounds analyzed showed similar recovery yields at 30 and 40 °C and were
264 stable during all extraction times.

265 **Effect of the oil/solvent ratio**

266 Different ratios of VOO: Xyl/ChCl-NADES (1:1, 1:3, 1:4 and 1:7) were used in order to
267 determine the influence of the oil/solvent ratio on the yield of phenolic compounds
268 extracted using the control conditions of 1 h at 40 °C. The 1:1 ratio extracted significantly
269 higher concentrations of the secoiridoids 3,4-DHPEA-EDA, *p*-HPEA-EDA and 3,4-
270 DHPEA-EA (Fig. 4a), yielding 22.5%, 31.7% and 46 % higher mean concentrations than
271 for ratios of 1:3, 1:4 and 1:7, respectively. The alcohols Hy and Ty showed similar
272 behavior, with the 1:1 ratio producing the most efficient extraction (Fig. 4b). However,
273 no significant differences ($p<0.05$) were found for the extraction of lignans and the
274 flavonoids between the different ratios assessed.

275 The highest phenolic extractive yields were obtained using the control conditions, 40 °C
276 during 1 h with a 1:1 VOO: Xyl/ChCl-NADES ratio (Table 1), with which a concentration
277 of 555.36 mg/kg VOO was obtained.

278 **Removal of solvent from the NADES extract**

279 To remove the solvent, the NADES extracts were passed through a column filled with
280 XAD-16 resin, the solvent was washed with deionized water with no acidification, and
281 the adsorbed phenols were eluted by organic solvent. The influence of the bed height,
282 acidity of the wash water and the solvent used for the desorption of phenols and its
283 concentration were analyzed.

284 In order to recover and concentrate the phenols from the NADES extracts, a
285 macrophorous adsorbent resin XAD-16 was used. To study the effect of height on the
286 adsorption capacity of the phenolic compounds from the NADES extract on the resin, 2
287 beds heights were assayed, 10 and 20 cm. Following adsorption, the adsorbate-laden
288 column was washed first by acidified and then non-acidified desionized water with the
289 objective of protecting the phenolic compounds until all the NADES was eluted
290 (Mylonaki et al. 2008). The effect of wash-water acidity on the recovery of phenolic
291 compounds was studied by washing a 10 cm and 20 cm bed height with acidified and
292 non-acidified wash water. Results showed no significant differences due to the 2 beds
293 heights of resin analyzed or to the wash-water acidity on the recovery of phenolics.

294 Significant difference were only found in the sum of phenolic compound recovery from
295 these extracts after washing with acidified water at a bed height of 10 cm, obtaining
296 555.36 mg/kg of phenols in these conditions and 447.08 mg/kg of phenols desorpting
297 with non-acidified wash water. A bed height of 10 cm and acidified water were used in
298 the following desorption assay.

299 Then a 100 mL sequential desorption with different concentrations of ethanol (50, 80 and
300 100%) was used in order to determine the effect of solvent concentration on the
301 polyphenol extraction yield. Table 2 shows the concentration of simple phenols,
302 secoiridoids, lignans and flavonoids recovered at the different ethanol concentrations. It
303 should be noted that the most polar compounds, the simple phenols Hy and Ty, were
304 recovered in higher proportions (81.7% and 83.6%), with the lowest concentrations of
305 ethanol, 50% and 80%, respectively. The most abundant compounds present in the olive
306 oil studied, 3,4-DHPEA-EDA and *p*-HPEA-EDA, remained in the resin in high
307 proportions (26.8-31.5% of the total amount recovered) after elutions with 50% and 80%

308 ethanol; it was necessary to increase the ethanol concentration to 100% for their complete
309 recovery. Less polar compounds 3,4-DHPEA-EA, *p*-HPEA-EA, luteolin and apigenin
310 were recovered in high proportions 93.4%, 69%, 96% and 98%, respectively after elution
311 with 80% and 100% ethanol. However, the desorption of lignans, 1-acetoxypinoresinol
312 and pinoresinol, with a similar polarity according to their behavior in HPLC under the
313 conditions of this study, showed a similar trend and reached maximum values at an
314 ethanol concentration of 100%. The content of lignan remained low even at high ethanol
315 concentrations, with a concentration of 100% ethanol necessary to recover 74.9% and
316 78.3% of 1-acetoxypinoresinol and pinoresinol, respectively. Therefore, 100% ethanol
317 was selected as the appropriate desorption solution for all the phenolic compounds
318 extracted with NADES from VOO. When 100% methanol was used as elution solvent,
319 the amounts of recovered phenolic compounds were statistically similar ($p < 0.05$) to those
320 eluted with 100% ethanol, except for 3,4-DHPEA-EDA. Bertin et al. (2011) found the
321 highest desorption rates were obtained with ethanol, which mobilized almost all
322 polyphenols adsorbed onto XAD-16 resins. Thus, all the solvents used in this extraction
323 process are “green” solvents, such as water and ethanol. Moreover, the NADES could be
324 reused several times, reducing the associated cost of the extraction process.

325 **Conclusion**

326 The present work reports an effective method for the extraction of phenolic compounds
327 from VOO using NADES based on xylitol and ChCl, as well as the recovery of the
328 phenolic compounds and the removal of NADES from a macroporous resin was
329 developed. The most effective extraction conditions were 1 h at 40 °C with a VOO:
330 Xyl/ChCl ratio of 1:1 for the highest percentage extraction of all the phenolic compounds
331 without degradation. The most efficient conditions for the recovery of phenolic

332 compounds and removal of NADES-based Xyl/ChCl was a column bed height of 10 cm,
333 250 mL of acidified wash water and 300 mL of ethanol as eluent, which allowed the
334 recovery of a total of 555.36 mg/kg phenolic compounds. These results are comparable
335 to those obtained by direct analysis of phenols without removal of NADES whose sum
336 was 527.36 mg/kg of phenols. This indicates that no phenols were significantly lost in the
337 solvent removal process under these conditions. This work presents an eco-friendly and
338 highly efficient method for the extraction of phenolic compounds from VOO, and their
339 recovery and concentration from NADES.

340

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344

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Table 1 Sum of the polyphenol content (mg/kg) obtained with the different assayed conditions: temperature (30, 40, 60 and 90° C), time (0.5, 1, 2 and 6 h at 30° and 40° C), and VOO: Xyl/ChCl-NADES ratio (1:1, 1:3, 1:4 and 1:7).

Temperature	time of extraction 1h, VOO:NADES ratio (1:1)		
30 °C	477.11 ± 0.110	c	
40 °C	555.36 ± 21.93	d	
60 °C	408.00 ± 26.69	b	
90 °C	345.93 ± 254.58	a	
Time	VOO:NADES ratio (1:1)		
	temperature of extraction 30 °C		temperature of extraction 40 °C
0,5 h	430.08 ± 5.42	c	466.47 ± 1.554
1 h	477.11 ± 0.10	d	555.36 ± 21.93
2 h	420.71 ± 25.81	c	333.03 ± 18.99
6 h	351.84 ± 14.42	b	313.92 ± 4.86
Ratio VOO:NADES	temperature of extraction 40 °C, time of extraction 1 h		
1:1	555.36 ± 21.93	b	
1:3	422.04 ± 21.55	a	
1:4	428.52 ± 356.01	a	
1:7	400.68 ± 4.43	a	

Values are expressed as mean ± SD (n=2). One-way ANOVA ($p < 0.05$). In each experiment the value of different treatments followed by different letters are significantly different according to the Duncan test ($p < 0.05$).

Table 2 Polyphenol content (mg/kg) expressed as a function of the concentration of ethanol used on desorption on column and percentage of recovery of phenolic compounds (% R). The conditions used to extract the phenolic compounds from 14 g of VOO were, extraction time of 1 h, temperature 40 °C, VOO: Xyl / ChCL-NADES ratio (1: 1). For the recovery of the phenolic compounds, a column bed height of 10 cm of XAD-16 resin was used, pre-treated with 50 mL of ethanol followed by 50 mL of acidified water, washed with 250 mL of acidified water and a sequential desorption was performed with 100 mL of 50, 80 and 100% ethanol.

Phenolic compounds	EtOH 50%		EtOH 80%		EtOH 100%	
	Mean±SD	% R	Mean±SD	%R	Mean±SD	% R
Hydroxytyrosol	2.62 ± 3.09 ^a	21.27	7.44 ± 2.75 ^a	60.39	2.26 ± 0.9 ^a	18.34
Tyrosol	0.96 ± 1.06 ^a	16.90	3.79 ± 1.52 ^a	66.73	0.93 ± 0.28 ^a	16.37
3, 4- DHPEA-EDA	19.33 ±15.18 ^a	10.02	121.91 ± 12.78 ^b	63.16	51.77 ± 10.38 ^a	26.82
<i>p</i> -HPEA-EDA	1.95 ± 0.12 ^a	3.02	42.18 ± 0.47 ^c	65.42	20.35 ± 1.03 ^b	31.56
3,4-DHPEA-EA	2.00 ± 0.35 ^a	7.32	13.16 ± 0.36 ^b	48.9	12.15 ± 1.72 ^b	44.49
<i>p</i> -HPEA-EA	1.48 ± 0.19 ^{ab}	30.14	0.12 ± 0.04 ^a	2.44	3.31 ± 1.06 ^b	67.41
1-acetoxypinoresinol	1.84 ± 0.07 ^b	17.31	0.83 ± 0.04 ^a	7.81	7.96 ± 0.54 ^c	74.88
Pinoresinol	0.12 ± 0.01 ^a	14.46	0.06 ± 0.01 ^a	7.23	0.65 ± 0.14 ^b	78.31
Luteolin	0.33 ± 0.07 ^a	4.47	4.42 ± 1.61 ^b	59.89	2.63 ± 0.03 ^{ab}	35.64
Apigenin	0.04 ± 0.04 ^a	2.26	0.66 ± 0.17 ^b	37.29	1.07 ± 0.02 ^c	60.45

Values are expressed as mean ± SD (n=2). Means with different superscript letters in every line are significantly different according Duncan test ($p < 0.05$).

Figure Captions

Fig. 1 HPLC chromatogram of phenolic compounds in virgin olive oil and their concentrations extracted by NADES using a time of extraction of 1 h, ratio of virgin olive oil: NADES (1 : 1), temperature 40 °C. Direct injection of the NADES extract (**a**), concentration of the extract and solvent removal with 10 cm of XAD-resin bed height, washing with acidified water, and desorption with 300 ml of ethanol 100 % (**b**). The concentrations are expressed as mg/kg of VOO \pm SD (n = 2).

Fig. 2 Effect of temperature on the concentration of phenolic compounds in virgin olive oil (VOO). (**a**) oleacein (3,4-DHPEA-EDA); oleocanthal (*p*-HPEA-EDA); oleuropein aglycon (3,4-DHPEA-EA) and ligstroside aglicon (*p*-HPEA-EA). (**b**) hydroxytyrosol (Hy), tyrosol (Ty), 1-acetoxypinoresinol, pinoresinol, luteolin, apigenin. The results are expressed as mg/kg of VOO \pm SD (n = 2). The letters represent significant differences, absence of letters indicate non-significant differences according to Duncan's test ($p < 0.05$).

Fig. 3 Effect of the extraction time on the concentration of the phenolic compounds in virgin olive oil (VOO). At 30 °C and 40 °C. (**a**), (**c**) oleacein (3, 4-DHPEA-EDA); oleocanthal (*p*-HPEA-EDA); oleuropein aglycon (3, 4-DHPEA-EA) and ligstroside aglicon (*p*-HPEA-EA). (**b**), (**d**) hydroxytyrosol (Hy), tyrosol (Ty), 1-acetoxypinoresinol, pinoresinol, luteolin, apigenin. The results are expressed as mg/kg of VOO \pm SD (n = 2). The letters represent significant differences, absence of letters indicate non-significant differences according to Duncan's test ($p < 0.05$).

Fig. 4 Effect of ratio virgin olive oil (VOO): Xyl/ChCl-DES on the concentration of phenolic compounds in VOO. **(a)** oleacein (3, 4-DHPEA-EDA); oleocanthal (*p*-HPEA-EDA); oleuropein aglycon (3,4-DHPEA-EA) and ligstroside aglicon (*p*-HPEA-EA). **(b)** hydroxytyrosol (Hy), tyrosol (Ty), 1-acetoxypinoresinol, pinoresinol, luteolin, apigenin. The results are expressed as mg/kg of VOO \pm SD (n = 2). The lowercase letters represent significant differences, absence of letters indicate non-significant differences according to Duncan's test ($p < 0.05$).

Figure 1

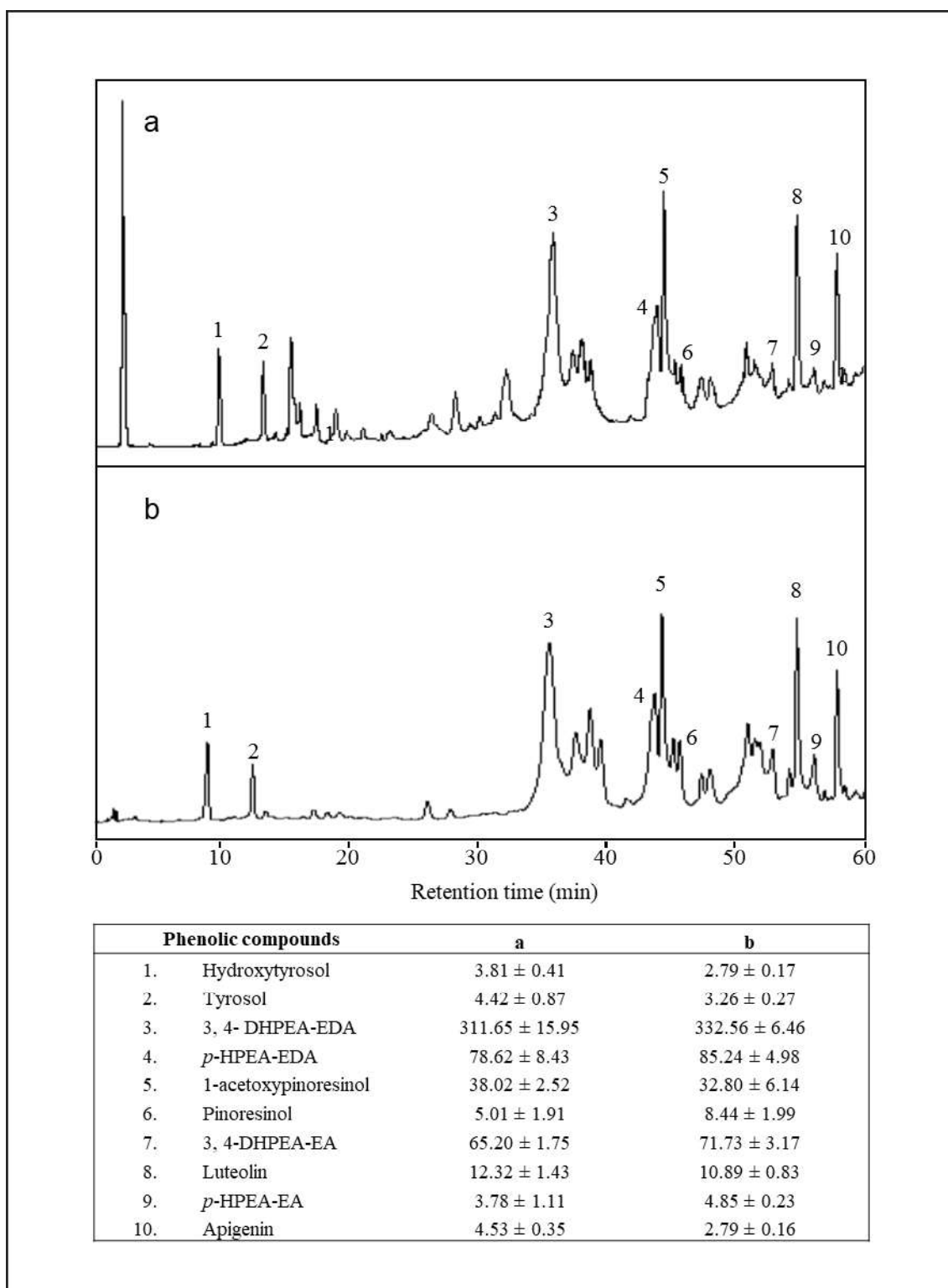


Figure 2

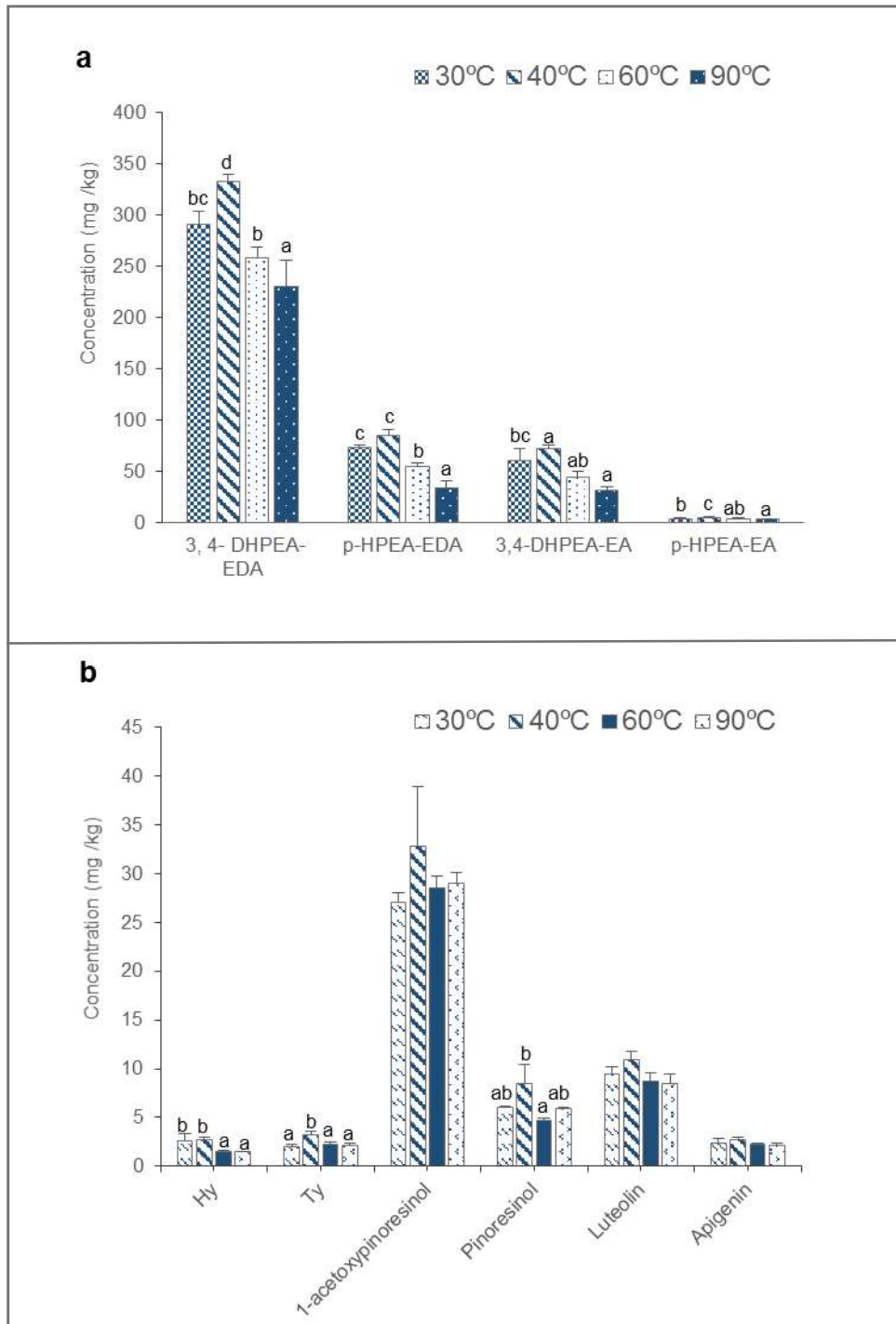


Figure 3

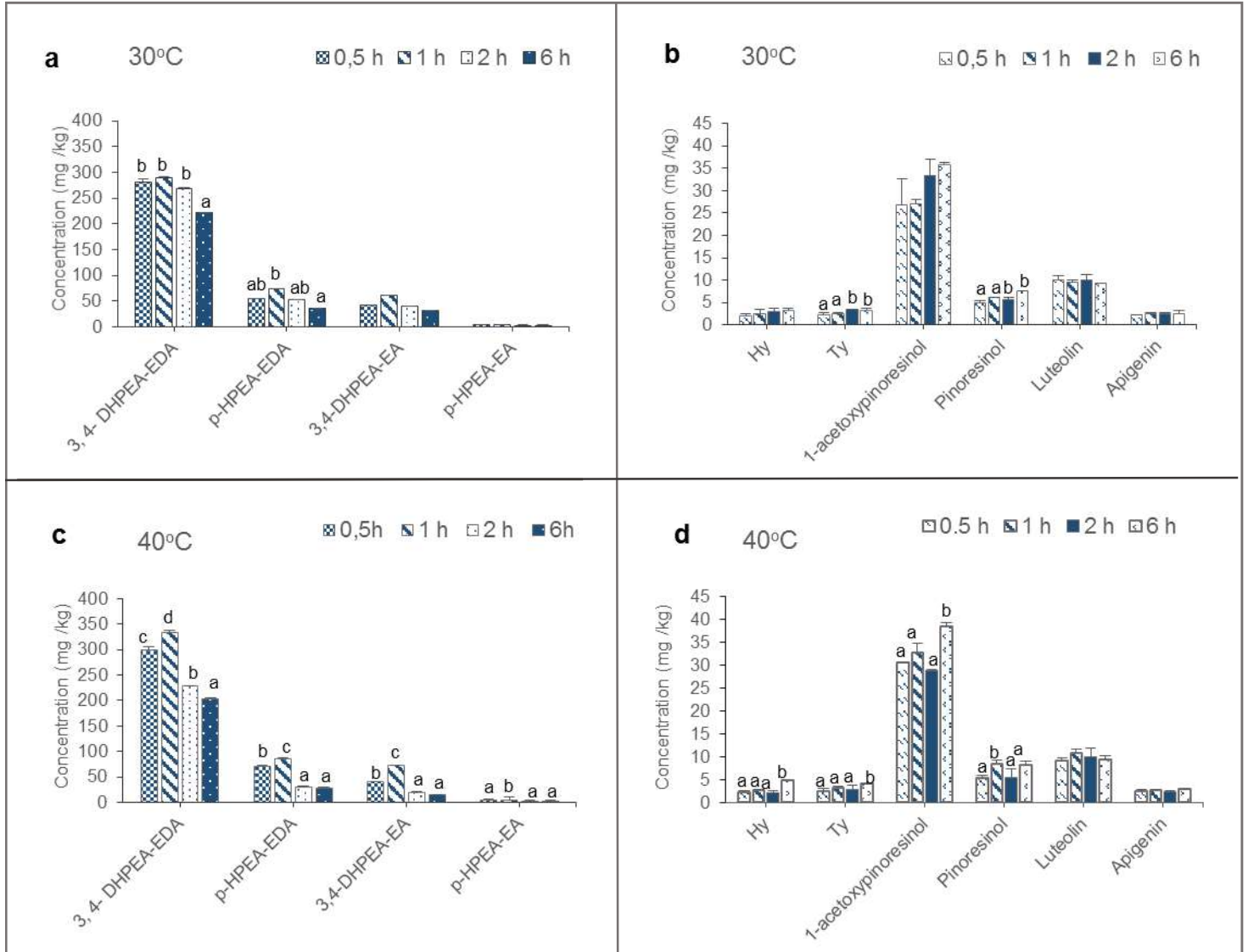
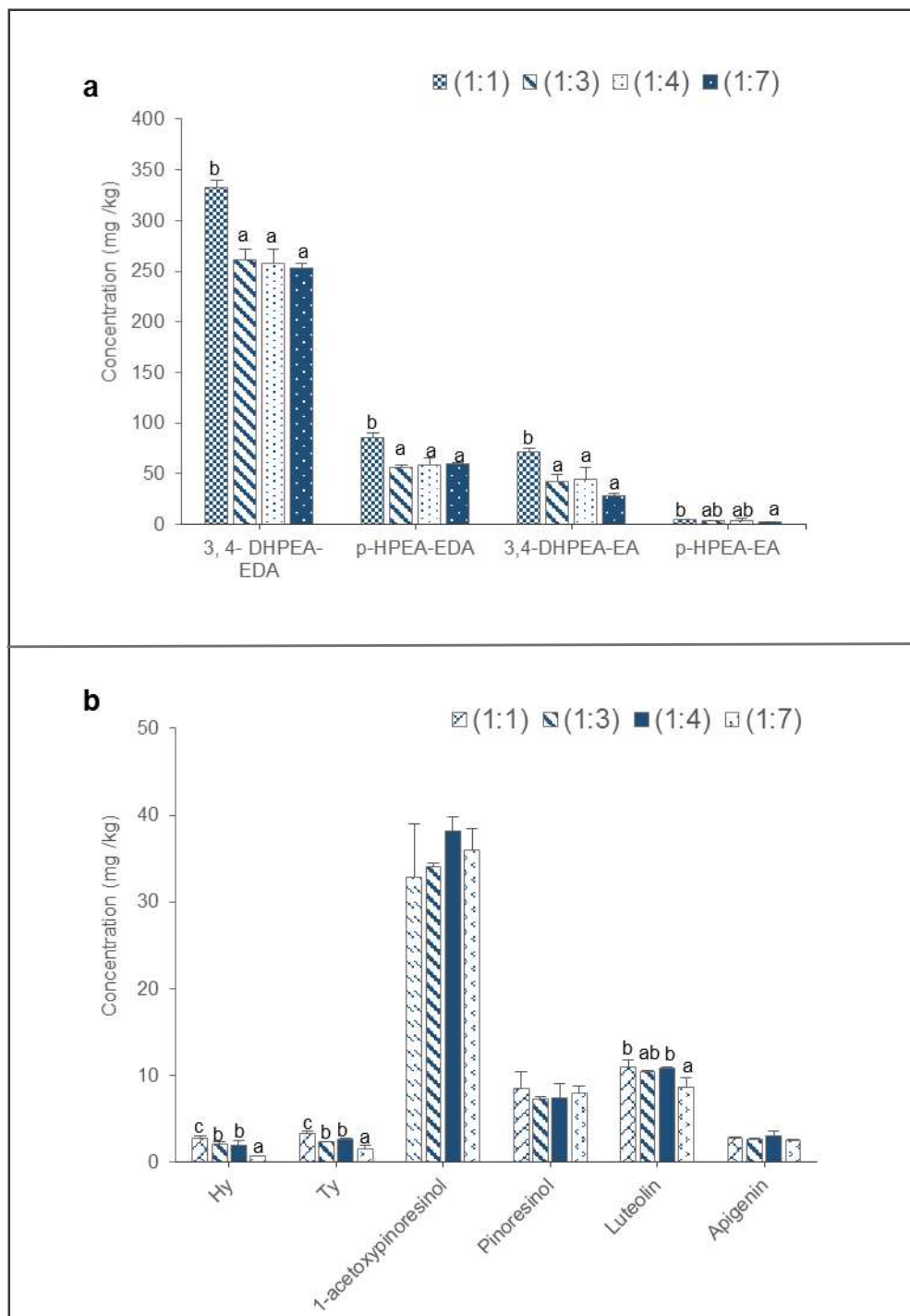
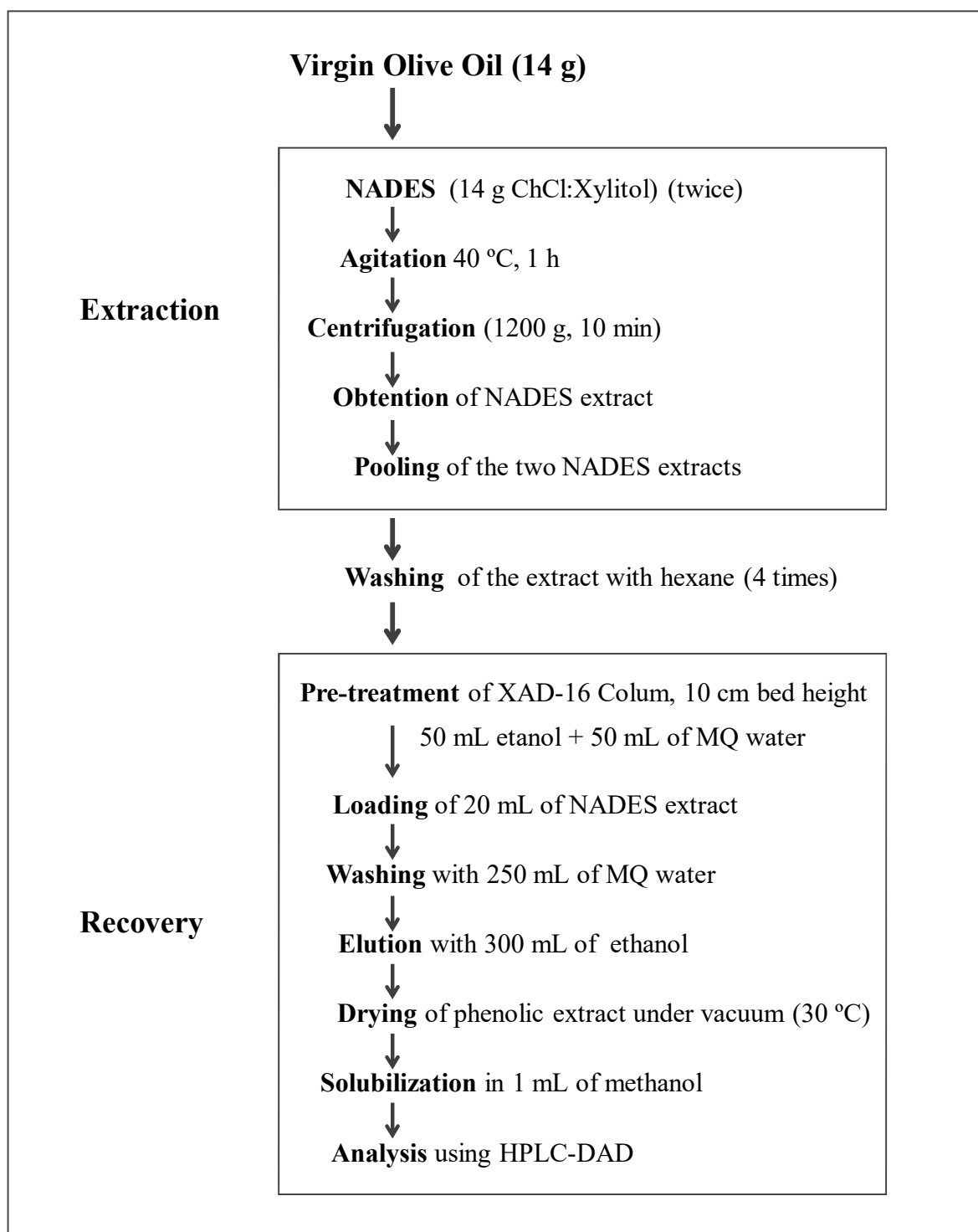


Figure 4





Extraction and recovery of phenolic compounds from virgin olive oil under the control conditions.

Phenolic compounds from virgin olive oil obtained by natural deep eutectic solvent (NADES): effect of the extraction and recovery conditions

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